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Anne Pommier, Fabrice Gaillard, Michel Pichavant

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**TIME-DEPENDENT CHANGES OF THE ELECTRICAL
CONDUCTIVITY OF BASALTIC MELTS
WITH REDOX STATE**

POMMIER A.¹, GAILLARD F.¹ AND PICHAVANT M.¹

¹ *CNRS/INSU, Université d'Orléans, Université François Rabelais-Tours,
Institut des Sciences de la Terre d'Orléans (ISTO), UMR 6113,
Campus Géosciences, 1A rue de la Férollerie,
45071 Orléans cedex 2, France*

Abstract 300 better)

The electrical conductivity of basaltic melts has been measured in real-time after fO_2 step-changes in order to investigate redox kinetics. Experimental investigations were performed at 1 atm in a vertical furnace between 1200°C and 1400°C using air, pure CO_2 or CO/CO_2 gas mixtures to buffer oxygen fugacity in the range 10^{-8} to 0.2 bars. Ferric/ferrous ratios were determined by wet chemical titrations. A small but detectable effect of fO_2 on the electrical conductivity is observed. The more reduced the melt, the higher the conductivity. A modified Arrhenian equation accounts for both T and fO_2 effects on the electrical conductivity. We show that time-dependent changes in electrical conductivity following fO_2 step-changes monitor the rate of Fe^{2+}/Fe^{3+} changes. The conductivity change with time corresponds to a diffusion-limited process in the case of reduction in $CO-CO_2$ gas mixtures and oxidation in air. However, a reaction at the gas-melt interface probably rate limits oxidation of the melt under pure CO_2 . Reduction and oxidation rates are similar and both increase with temperature. Those rates range from 10^{-9} to $10^{-8}m^2/s$ for the temperature interval 1200-1400°C and show activation energy of about 200kJ/mol. The redox mechanism that best explains our results involves a cooperative motion of cations and oxygen, allowing such fast oxidation-reduction rates.

1. INTRODUCTION

Several studies have revealed the important controls of redox potential, usually quantified as oxygen fugacity (fO_2), on metal/silicate melt, crystal/melt and gas/melt equilibria (Carmichael and Ghiorso, 1990; Righter and Drake, 1996; Moretti and Papale, 2004; Gaillard and Scaillet, 2009). This makes redox condition of basaltic melts one of the most critical parameter influencing many planetary processes, involving core formation, mantle melting and metasomatism, crystallization of magmas and magma degassing (Righter and Drake, 1996; Herd, 2008; Frost and McCammon, 2008). Several multivalent elements determine the fO_2 of basaltic melts (Fe, C, H, O, S), but the ferric/ferrous ratio of the melt is commonly used to monitor redox changes in magmatic processes (Kress and Carmichael, 1991; Behrens and Gaillard, 2006). The oxygen fugacity of a basalt is generally defined relatively to the one of a solid buffer, such as, from the more reducing to the more oxidizing, Iron-Wustite (IW), Quartz-Fayalite-Magnetite (QFM), Nickel-Nickel Oxide (NNO) (Herd, 2008).

Present-day basaltic lavas on Earth display a range in oxygen fugacity from 3 log-units below NNO to 4 log-units above NNO, corresponding to ferric/total iron ratios ranging from less than 10 to ~70% (Botcharnikov et al., 2005; Carmichael, 1991). Martian basalts record more reduced oxygen fugacities, ranging from 0.5 log-units to 3.5 log-units below NNO (Herd et al., 2002). Such variations in planetary basalts oxygen fugacity might reflect fundamental heterogeneities in the redox state of their source region but fO_2 can be also modified during melting, crystallization and degassing processes. Since such modifications can be kinetically controlled, a correct interpretation of fO_2 variabilities requires the understanding of the mechanisms and rate of changes in the redox potential in basalts. In this paper, we use electrical conductivity measurements to further document mechanisms and kinetics of redox changes in basaltic melts.

2. PREVIOUS WORKS

Mechanisms of oxidation/reduction of silicate melts have been actively investigated (e.g. Schreiber et al., 1986 and references therein). In H-bearing and H-free basaltic systems, reduction/oxidation reactions are commonly associated with the development of redox reaction fronts and are diffusion-limited (Wendlandt, 1991; Cooper et al., 1996a, b; Everman and Cooper, 2003; Gaillard et al., 2003a). For H-bearing systems, Gaillard et al. (2003b) calculated that H_2 mobility should rate-limit redox changes in basalts. In H-free systems, different rate-limiting species have been proposed. Oxidation-reduction reactions have been initially associated to the diffusion of oxygen (self-diffusion of oxygen; Wendlandt, 1991). However, self-diffusion experiments do not involve gain or loss of oxygen (^{16}O - ^{18}O substitutions are involved) whereas redox experiments implicitly require a change in the oxygen/cations ratio. Variable-valence ions have been found to enhance oxygen fluxes (Beerkens and de Waal, 1990). Redox experiments are usually related to oxygen (O_2) chemical diffusion experiments (Schreiber et al., 1986). For glasses or melts of similar composition, oxygen tracer diffusivity (D^*) is commonly several orders of magnitude slower than oxygen chemical diffusivity (D , Schreiber et al., 1986; Cook et al., 1990; Wendlandt, 1991) (Appendix 1). Such discrepancies between O diffusion coefficients have been interpreted in terms of different transport mechanisms, oxygen self- or tracer diffusion involving mobility of discrete cation-oxygen species within the melt while oxygen chemical diffusion is dominated by the migration of cationic species. Cooper et al. (1996b) have demonstrated that the diffusion of an oxygen species is not required during redox reactions in

melts and that the change in the oxygen/cations ratio is best accommodated by cations rather than oxygen diffusivity due to their greater mobility.

Oxygen self and chemical diffusion studies performed on synthetic (Sasabe and Goto, 1974; Dunn, 1982; Schreiber et al., 1986; Cook et al., 1990; Cook and Cooper, 2000; Reid et al., 2001) and natural silicate melts (Dunn, 1983; Canil and Muehlenbachs, 1990; Wendlandt, 1991; Cooper et al., 1996a) have demonstrated the dependence of both kind of diffusion mechanisms on the melt structure. This was also confirmed by other studies of iron redox reactions (e.g. Magnien et al., 2008). All that tends to underline that the Network Formers (Si, Al) lower the oxygen diffusivity (D) whereas the Network Modifiers (divalent cations and alkali) have the opposite effect. In basaltic melts, oxygen self-diffusion data were found to be comparable to divalent cations diffusivities. For example, in a basaltic melt at 1300°C, Muehlenbachs and Kushiro (1974) and Leshner et al. (1996) measured oxygen diffusivities (D^*) of $\sim 4.10^{-12}$ m²/s and 6.10^{-12} m²/s, respectively. This result questions the assumption of Cooper et al. (1996a, b) that $c_{O_2} \cdot D_{O_2} \text{ (and } c_{O_2} D_{O_2}) < c_{\text{modifier cations}} D_{\text{modifier cations}}$, c_x being the concentration of x.

The electrical conductivity, σ , reveals the mobility of the charge carriers in presence of a gradient in electrical potential and is an efficient probe of mass transfer processes within silicate melts and magmas. Previous studies have shown that it is extremely sensitive to many parameters, including temperature (T), pressure (P), melt composition (Tyburczy and Waff, 1983, 1985; Gaillard, 2004; Gaillard and Iacono Marziano, 2005; Pommier et al., 2008). However, the dependence of electrical conductivity of silicate melts to redox conditions has remained poorly documented. The only study on the subject (Waff and Weill, 1975) found no significant variation in σ with fO_2 and suggested to neglect the influence of fO_2 on the electrical properties of silicate melts.

We have undertaken a systematic investigation of the influence of fO_2 on the electrical response of two different basaltic melts at 0.1MPa and different temperatures. The study was motivated by (1) the need to reexamine the conclusions of Waff and Weill (1975) in the light of recent methodological advances in the field of electrical measurements and (2) the need to understand redox kinetics and mechanisms in natural silicate melts, the electrical conductivity being here used as a probe for investigating mass transfer properties. Modern techniques of measurements of electrical conductivity such as impedance spectroscopy (Huebner and Dillenburg, 1995) allows the electrical response to be separated in terms of an imaginary and a real part, the latter corresponding unambiguously to the electrical resistance of the sample. In the case of oxidation/reduction reactions, the real time electrical response of the melts was not monitored in previous studies (Waff and Weill, 1975) and is therefore unknown. In our study, the

electrical conductivity was continuously measured from step changes in fO_2 until the attainment of redox equilibrium. In turn, this allows conductivity changes to be interpreted in terms of kinetics and mechanisms of redox changes in the melt. Equilibrium conductivities were extracted from the evolution of σ -time plots and used to establish the dependence of the electrical conductivity with fO_2 for the two basaltic melts and different temperatures investigated. The conductivity measurements were complemented by major element and FeO analyses of experimental glasses in order to relate the electrical and redox state of the studied melts. For most experiments, the kinetics of the electrical response can be satisfactorily fitted by a diffusion formalism, suggesting that both oxidation and reduction reactions are kinetically limited by diffusion. The high values of the calculated diffusion coefficients ($\sim 10^{-9} \text{ m}^2/\text{s}$ for our investigated T range) can be explained by redox mechanisms involving both oxygen and cations fluxes.

3. EXPERIMENTS

3.1. Starting products

The starting materials are two different basalts: one collected from the active vent of Pu'u' 'O'o volcano (Kilauea, Hawaii) in 2007 and a tephrite (VES9) coming from a 8th century eruption of Mt. Vesuvius (Italy). Chemical analyses of the starting glasses are given in Table 1. Each rock was finely crushed in an agate mortar. The powder was dried and then melted in air at 1400°C during ~1h. Therefore, all starting glass samples were prepared under strongly oxidizing conditions ($\log fO_2 = -0.69$). Quenching resulted in bubble-free glasses that were drilled to cylinders (6 mm OD, 6.5-10 mm length), and directly loaded in the electrical conductivity cell. NBO/T ratios (number of non-bridging oxygens divided by number of tetrahedral cations) of the two glasses, calculated considering Fe as both FeO and Fe₂O₃ and neglecting the presence of Ti (Mysen and Richet, 2005), are 0.56 for the Kilauea basalt and 0.55 for the Mt. Vesuvius tephrite. This underlines a similar polymerization of the tephrite and the basalt.

3.2. Experimental setup

All experiments were performed in a one atmosphere vertical furnace. Experimental temperatures ranged from 1200 to 1400°C. Temperature, monitored with a *Eurotherm* controller, was measured by a type-S thermocouple, placed adjacent to the conductivity cell, and is known to within +/- 2°C. The sample and the thermocouple were both located in the 3 cm hot spot of the

furnace. Experimental redox conditions were controlled by the gaseous atmosphere present in the furnace. Three types of gaseous atmospheres were employed: air, pure CO₂ and CO-CO₂ mixtures. Note that experiments using only CO₂ are never performed under pure CO₂, since a small quantity of CO is always present in the gas bottle. This small amount of CO (in general < a few tens of ppm) allows the gas atmosphere to act as a buffer.

For air, the tube furnace was left open to the ambient atmosphere. In contrast, for both CO₂ and CO-CO₂ mixtures, gases were flown through the furnace (typical flow rates were 200cc/min). For CO-CO₂ mixtures, three different gas proportions (39.7% CO₂/1.6% CO; 38.8% CO₂/5.9% CO; 36.5% CO₂/17.5% CO) were imposed using electronic flowmeters. Redox conditions (fO₂) were calculated from Deines et al. (1974) and directly measured using a zirconia electrolyte cell. These are referenced against the Ni-NiO equilibrium at 0.1MPa (Pownceby and O'Neill, 1994). For pure CO₂ gas, ΔNNO values range from 3.45 to 4.00 (Table 2 and 3); for CO-CO₂ gas mixtures, ΔNNO values divide into three groups (0.75-1.40; -0.35-0.45; -1, Table 2 and 3), depending on the specific gas mixture imposed.

Conductivity measurements were performed using a two-electrode configuration on cylindrical samples (Gaillard, 2004; Pommier et al., 2008, Figure 1a). Glass samples of 6mm OD and 8-9mm length were typically used. The inner electrode of the conductivity cell is a 1mm Pt wire inserted in the center of the glass sample and the external electrode is a Pt tube surrounding the sample. The drilled alumina ceramic part located at the bottom of the conductivity cell prevents the two electrodes from being in contact (Figure 1a). This configuration ensures the stability of the cell during the experiment. We assume that no convection occurs in the samples since the Rayleigh number is very small (<200, Jaupart and Tait, 1995), due to the small dimensions of the samples. Thermodiffusion (Soret effect) requires the presence of a thermal gradient, which is not the case in our experiments (thermal gradient <1-2°C). At the end of the experiment, the conductivity cell and the sample were removed from the furnace and allowed to cool down under room conditions. Quenched glasses from selected conductivity charges were collected and prepared for FeO titration and electron microprobe analyses.

3.3. Experimental strategy

For each experiment at a given temperature, two fO₂ steps were performed. Electrical measurements were recorded continuously until the attainment of the different equilibrium redox states. Reduction experiments consisted in an initial relatively oxidizing step followed by a final step under more reducing conditions. Oxidation experiments were the reverse of reduction

experiments: an initial relatively reducing step was followed by a more oxidizing step. In practice, fO_2 changes were obtained by switching either from air or pure CO_2 to $CO-CO_2$ mixtures (reductions), or from $CO-CO_2$ mixtures to air or pure CO_2 (oxidations). On the basis of voltage measurements using the zirconia probe, changing fO_2 from $CO-CO_2$ to pure CO_2 or air and reciprocally takes approximately a few minutes. Electrical measurements during this transition period were discarded. For oxidations in air, the conductivity cell was taken out of the furnace during the evacuation of the $CO-CO_2$ gas mixture and then replaced in the furnace at T. Durations for each fO_2 steps ranged between 90 and 1900min (Table 2).

In parallel to electrical conductivity experiments, experiments were performed in order to determine Fe^{2+}/Fe^{3+} and other chemical changes associated with the real-time evolution of the oxygen fugacity. These experiments (designated below as analytical experiments, Table 3) used the same sample configuration and dimensions as the conductivity experiments (Figure 1b). Similarly, only one end of the glass cylinder was in contact with the furnace atmosphere. T and fO_2 conditions were selected to match those in conductivity experiments. Samples have been rapidly quenched before redox equilibrium, as monitored from the electrical measurements, was attained. Experimental glasses were analyzed for FeO titration and electron microprobe analyses.

3.4. Acquisition and reduction of the electrical data

In this study, electrical conductivities were derived from complex impedance spectroscopy (Roberts and Tyburczy, 1994). Electrical impedances of samples were determined at variable frequencies using a Solartron 1260 Impedance Gain Phase Analyzer, (Schlumberger Co.), equipped with Zview software package (Huebner and Dillenburg, 1995; Gaillard, 2004; Maumus et al., 2005). Each measurement consisted in a scan in frequency from 1 Hz to 10^6 Hz, lasting typically about 1min. For each frequency, the complex impedance was recorded. The experimental procedure, including details on the calibration process, is detailed in Pommier et al. (2009, in press). The reproducibility of the data has been demonstrated in Pommier et al. (2008).

The complex impedance, Z, can be written as the sum $Z'+jZ''$, with Z' the real part and Z'' the imaginary part of Z (and $j^2=-1$). The electrical response of the sample to a scan in frequency is directly observed in the Nyquist plane (Z', Z'') (Figure 2), from which the value of the electrical resistance R is deduced (e.g. Huebner and Dillenburg, 1995). The non semi-circle shape of the impedance spectra is due to the fact that the samples are very conductive on the investigated T range, implying their electrical resistance to be smaller than the inductive effects

($Z'' < 0$). The corresponding electrical conductivity value σ is then deduced using the geometric factor G (Gaillard, 2004; Pommier et al., 2008):

$$\sigma = (G.R)^{-1} \quad (1)$$

The geometric factor varies from 0.022 to 0.037 m. The uncertainty on σ due to error propagation of typical uncertainties on R (R is known to ± 0.5 ohm in the investigated T range), L, d_{ext} and d_{int} (uncertainties on the length and the two diameters are 0.1mm) is in the range of 4.7-9% for both our Kilauea and Mt. Vesuvius samples.

For fixed T and fO_2 conditions and for each starting glass composition, time series measurements were conducted. They consisted in the successive acquisition of electrical measurements (each comprising a scan in frequency from 1 Hz to 10^6 Hz) until a stable value of R (and, thus, of σ) was reached (plateau values). The time interval between two electrical measurements ranged from 30 s to 1 hr depending on the evolution of the electrical response with time: at the beginning of the experiment, small time intervals were required since the electrical response changed rapidly; on the contrary, at the end of the experiment, the small changes in the electrical response (plateau values) allowed the use of longer time spans.

3.5. Analytical techniques

Experimental glasses were observed optically under a microscope, in order to check for the presence of crystals and bubbles. Crystals were found to be present in some oxidation experiments performed at 1200°C in air for the Kilauea basalt. Results from these experiments were discarded and are not presented.

A Camebax SX-50 electron microprobe (BRGM-CNRS-Université d'Orléans) was used to analyze both the starting and the experimental glasses. Analyses were conducted at 15kV, 6nA, 10s on peak and 5s on background. Both spot analyses and traverses were performed. Traverses served to evaluate the degree of iron loss from the melt to the Pt electrodes and the extent of Al^{3+} incorporation and diffusion from the ceramic part of the conductivity cell into the melt (Figure 1b). In the analytical charges, EMPA traverses at the gas/melt interface were used to determine the type and importance of major elements fluxes to redox changes (see Figure 1).

The FeO concentration of the starting and experimental glasses was determined by colorimetric redox titration (Gaillard et al., 2003b). With this method, the sample is dissolved in $HF + H_2SO_4$ solution and the titration is then performed using a potassium dichromate solution. The equivalence volume provides the value of the concentration of FeO. At least 25mg of

sample powder were used for the titration in order to ensure accuracy and reproducibility. The Fe_2O_3 concentration is then calculated from:

$$\text{Fe}_2\text{O}_3 = 1.1113 \cdot (\text{FeO}_{\text{tot}} - \text{FeO}), \quad (2)$$

where Fe_2O_3 is the concentration in ferric iron (wt%), FeO_{tot} is the total iron concentration (wt%) measured by electron microprobe and FeO is the concentration of ferrous iron (wt%) determined as above. FeO and Fe_2O_3 concentrations are then used to calculate the at. $\text{Fe}^{2+}/\text{Fe}^{3+}$ ratio.

4. RESULTS

4.1. Melt-conductivity cell interactions

Spot electron microprobe analyses performed in the center of the glass cylinders in most cases showed no significant changes in major element oxides in comparison with starting glass compositions. Exceptions were experiments performed at the lowest temperatures (1200°C) for the Kilauea glass and at $\log f\text{O}_2 = -3.74$ and -0.69 ($f\text{O}_2$ in bar) (see Table 2). For those samples, the variations in major elements concentration can be explained by the crystallization of Fe-Ti-Mg oxides observed in the experimental glasses. These observations indicate that no noticeable alkali volatilization occurred during these redox experiments.

The glass-Pt interface shows no significant variations in oxide concentrations, except for FeO, as already observed by Pommier et al. (2008). On average, iron depletions range between 2 and 7% relative. A maximum depletion of 15% FeO relative affecting the melt on a distance <500microns was found only for the longest experiments, for which the experimental duration exceeded the average run duration by several hours. For instance, in experiment #5 (one of the longest experiments (Table 2), thus particularly exposed to Fe losses), the iron content close to the electrode is ~4.3% mol oxide against 4.6% mol oxide in the starting glass, corresponding to a decrease of 6.5% compared to the FeO content. Iron depletions affect a distance in the Pt electrode <100microns (Figure 3a), thus insignificantly modifying the iron content in the glass (Figure 3b). As a result, the bulk data (electrical conductivity and wet chemistry) will not be significantly affected by Fe losses to Pt electrodes.

The glass-alumina interface presents on most samples a nearly continuous 10-30 μm thick layer comprising Al-Mg-Fe spinel and some scattered plagioclase crystals. The contribution of these crystals to the measured electrical conductivity was evaluated according to the method exposed in Pommier et al. (2008). Calculations show that the contribution of the crystals is less than 1% of the measured conductivity.

4.2. Effect of oxygen fugacity and temperature on the electrical conductivity

Electrical conductivities of the Kilauea sample measured at temperatures ranging from 1200 to 1400°C and covering a range of oxygen fugacities of $10^{-7.7}$ to 0.2 bar are shown in Figure 4. These are steady-state values of electrical conductivity associated with chemical equilibrium at the set fO_2 . A small but clearly detectable effect of oxygen fugacity on the electrical conductivity is demonstrated for each isotherm. The more reduced the melt, the higher the electrical conductivity. For comparison, no effect of fO_2 on the electrical conductivity was observed in the study of Waff and Weill (1975). For both Kilauea and Vesuvius samples, the change in electrical resistance following a change in redox conditions is about a few ohms, largely exceeding the sensitivity of our measurements (better than 0.1%) at given T and fO_2 . A small effect of composition is observed, the VES9 sample being less conductive than the Kilauea sample at 1200 and 1300°C (σ_{eq} values in Table 2).

At 1300°C, for the Kilauea sample, a change in fO_2 of 8 log-units modifies the electrical conductivity of ~0.2 log-unit (Figure 4). A similar effect is observed at the other investigated temperatures. For a given fO_2 , the electrical conductivity increases with temperature (Figure 4). The influence of temperature (increase of ~1.2 log units from 1200 to 1400°C) appears to be similar at low and high fO_2 . This temperature dependency of the conductivity can be fitted by an Arrhenius equation:

$$\sigma = \sigma_0 \cdot \exp\left[\frac{-Ea_\sigma}{RT}\right] \quad (3)$$

with σ the electrical conductivity (ohm.m^{-1}), σ_0 the pre-exponential factor (ohm.m^{-1}), Ea_σ the activation energy (J/mol), R the universal gas constant ($\text{J.K}^{-1}.\text{mol}^{-1}$) and T the temperature (K). Depending on the gas atmosphere, linear least-squares regression analysis of electrical data yields different activation energies that are presented in Table 4. Since a small effect of fO_2 on σ was detected in our experiments, we have introduced in the Arrhenian formalism the fO_2 parameter. Depending on both T and the redox conditions, the electrical conductivity of both Kilauea and Mt. Vesuvius melts can be expressed as

$$\sigma = (9.4.10^3) \cdot \exp\left[\frac{-117074}{RT}\right] \cdot (f_{O_2})^{-0.03} \quad (4)$$

Eq.4 reproduces measured conductivity values for all the experiments with a correlation coefficient of 0.93 and an average error of 11.6% relative.

4.3. Time-dependent changes in electrical conductivity during redox reaction

At a given temperature, the time necessary to reach a stable value of the conductivity (t_{eq}) following a change in redox state is approximately the same for a reduction under CO-CO₂ and an oxidation in air, while longer time spans are needed for oxidations under CO₂ (Table 2). At 1200°C, for both reduction and oxidation experiments, a stable (plateau) value of the conductivity is reached in more than 15hours, while less than 2hours are needed at 1400°C.

Results of typical reduction and oxidation (in air) experiments are presented in Figure 5a and 5b (experiments #6 and #15, respectively, Table 2). For both types of experiments, the exponential shape of the electrical response with time underlines similar reaction mechanisms and kinetics. For the experiment with pure CO₂ (Figure 5c), the electrical response is more linear with time, which contrasts with the curves obtained either for oxidation in air or for reductions in CO-CO₂. Changing the CO₂ flow rate in the furnace does not significantly change the shape of the electrical response with time (Figure 5c). The negligible effect of the gas flow rate on the kinetics of oxidation is in agreement with the observations made by Schreiber et al. (1986) using different air flow rates.

4.4. Variations in major element chemical concentrations

Electron microprobe traverses were performed in quenched samples from the analytical experiments to detect possible variations in major elements concentrations (Si, Al, Fe, Mg, Ca, Na, K) associated with redox changes. Traverses were performed in the longitudinal section of the samples, from the interface with gas to at least 4mm inside the glass sample (Figure 1b). The spatial resolution of the probe analyses is +/-5 microns.

Examples of microprobe traverses are presented in Figure 6 (traverses A and B: reductions; traverse C: oxidation). For clarity, we state here the presence of three parts in our samples (these parts will be interpreted Part 5 in terms of redox fronts): (1) The interface zone between gas and glass (<1mm depth), from the gas/sample interface to ξ' , is characterized by important variations in the concentration of network forming and network modifying cations in the quenched glass samples. ξ' is defined graphically and corresponds to the point at which the concentration of major elements presents an inflexion. For example, in experiment #6-QR (traverse A), this zone presents a relative increase of 5-8% in SiO₂ and Na₂O and 30% in K₂O and a decrease of 5-8% in MgO and CaO to 22% in FeO. (2) An inner zone begins at a depth >1mm (ξ') and extends as far as > 5 mm depending on experimental duration. It presents slight

fluctuations in alkali and Mg and Ca concentrations. In experiment #14-QO (traverse C), this zone presents an increase of 4% relative in CaO and MgO and a decrease of 8.8% relative in Na₂O. (3) A third zone, located near the bottom of the capsule, can be detected on some profiles (traverse B). This part of the sample is identified as the unreacted melt, the compositions in this zone corresponding to the starting glass compositions. Traverses performed on samples from conductivity experiments with duration exceeding t_{eq} have flat profiles for all major elements (traverse D).

4.5. FeO concentrations and evolution of glass Fe^{2+}/Fe^{3+}

Wet chemistry was used to determine the bulk value of Fe^{2+}/Fe^{3+} in glasses before and after most experiments (Tables 2 and 3). Analyses showed that the range of oxygen fugacities we investigated results in a range of $at. Fe^{2+}/Fe^{3+}$ of approximately 0.32 to 2.55 (Figure 7a).

The rate of change of Fe^{2+}/Fe^{3+} with time was documented in both reduction and oxidation experiments. Fe^{2+}/Fe^{3+} were measured at different time intervals following either a reduction (experiment #4, values at $t=0$, 300 and 1410min; #5, values at $t=0$, 45 and 1860min; #6, values at $t=0$, 45 and 430min) or an oxidation (experiment #12, values at $t=0$, 330 and 1380min; #14, values at $t=0$, 200 and 1300min) (Tables 2 and 3). For both reduction and oxidation, the rate of change of Fe^{2+}/Fe^{3+} is clearly nonlinear with time (Figure 7b). For example, oxidation in air of the Kilauea sample (experiment #14) shows a decrease in $at. Fe^{2+}/Fe^{3+}$ from 1.64 ($t=0$) to 0.52 at equilibrium ($t_{eq}=1300min$, Figure 7b). The intermediate value at $t=200min$ (0.83, Table 3) represents a change of ~80% toward the equilibrium value.

5. DISCUSSION

5.1. Ferrous / ferric ratio and electrical conductivity

5.1.1. Why does the ferrous/ferric ratio change the electrical conductivity ?

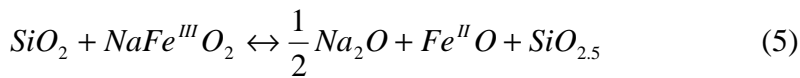
Sodium has been identified in several studies of electrical conductivity of natural melts as the main charge carrier (Tyburczy and Waff, 1983, 1985; Gaillard, 2004; Pommier et al., 2008). The contribution of the different ionic species (Na^+ , K^+ , Ca^{2+} , Mg^{2+} , Si^{4+} , Al^{3+} , O^{2-}) can be discriminated using the Nernst-Einstein equation (cf Gaillard, 2004, Pommier et al., 2008):

$$\sigma_i = \frac{D_i \cdot q_i^2 \cdot N_i}{k_B \cdot T \cdot H_r} \quad \sigma_{measured} = \sum_i \sigma_i$$

where D_i is the coefficient of diffusion of an ion i (m^2/s), q_i its charge (C), N_i the concentration of i (m^{-3}), k_B is the Boltzmann constant, T is the absolute temperature (K) and H_r the Haven ratio. D_i values are taken from Chakraborty (1995), calculated at 1300°C . For the Kilauea basalt, at 1300°C , this equation underlines that the contribution of sodium to the bulk conductivity is $\sim 80\%$, and the contribution of potassium is only 11% . This is coherent with the fact that the potassium cation is larger than Na and, thus, is supposed to diffuse in the melt with a slower rate than sodium. (usually, $D_{\text{Na}} \sim 10 \cdot D_{\text{K}}$, Chakraborty, 1995). The contributions of calcium and oxygen are 3% and 4% respectively. The contributions of Mg, Si and Al are $<1\%$. These calculations underline, in particular, that the contribution of divalent cations to the measured conductivity is negligible in an alkali-rich melt. The identification of sodium as the main charge carrier in our melts implies that the changes observed in the electrical response of the samples during a redox reaction (i.e. an increase in σ during a reduction, a decrease in σ during an oxidation) can be related to the modifications affecting the mobility of sodium.

Other mobile species that do not control the measured electrical conductivity of the melt (such as electrons or electron holes) are not supposed to significantly affect the shape of the impedance spectra. Thus, their possible contribution to the redox mechanisms can not be observed directly using the interpretation of spectra.

Structural studies have well established that alkali charge-compensate tetrahedrally coordinated cations such as ferric iron (e.g. Thornber et al., 1980; Dickenson and Hess, 1981; Mysen, 1983; Kress and Carmichael, 1988; 1991; Lange and Carmichael, 1989; Tangeman et al., 2001; Mysen and Richet, 2005). The charge-compensation reaction can be written in a structural way (Mysen and Richet, 2005) as follows:



where ferric iron is charge-compensated by sodium on the left hand-side of the equation. This equilibrium enlightens the double role of sodium, being either a charge compensator (left hand-side of the equation) or a network modifier (NM) (right hand-side). During an oxidation, the observed decrease in electrical conductivity most likely reflects a restricted mobility of sodium, since it is structurally associated to tetrahedrally coordinated units with ferric iron. On the contrary, under more reduced conditions, less of such units are present within the melt. Thus, sodium mobility is enhanced, consistent with the observed increase in electrical conductivity. It is important to note that Eq. 5 considers only part of ferric iron as NF and part of ferrous iron as

NM in the melt. Previous studies have shown that the presence of sodium in silicate melts promotes the formation of ferric iron (e.g. Kress and Carmichael, 1988).

5.1.2. Time evolution of the electrical conductivity and ferrous/ferric ratio

In our experiments, the temporal changes of both the electrical conductivity and the ferrous/ferric ratio have been monitored. To analyze these temporal evolutions, it is convenient to use the progress variable ϵ defined as (Crank, 1975; Wendlandt, 1991):

$$\epsilon(X) = (X(t) - X_0) / (X_{eq} - X_0) \quad (6)$$

with X being either σ or Fe^{2+}/Fe^{3+} , $X(t)$ the value of X at t , X_0 its initial value and X_{eq} its equilibrium value (plateau value). Both $\epsilon(\sigma)$ and $\epsilon(Fe^{2+}/Fe^{3+})$ are compared in Figure 8 for experiments #4 (values at $t=0$, 300 and 1410min), #5 ($t=0$, 45 and 1860min), #6 ($t=0$, 45 and 430min) and #14 ($t=0$, 200 and 1300min) (Tables 2 and 3). The data fall on the straight line 1:1. This single trend underlines that, during a redox reaction, the electrical conductivity and the ferric/ferrous ratio increase or decrease with the same rate. Thus, the evolution of the electrical conductivity with time is identical to that of the redox ratio of the melt. It follows that the time-dependence of the electrical response of the sample can be directly related to redox changes within the melt.

5.2. Determination of a bulk diffusion coefficient and transport properties

The experimental arrangement used in this study (Figure 1) is compatible with the mathematical model of the diffusion process applied to a plane sheet (Schreiber et al., 1986). In this model, diffusion occurs in a medium bounded by two parallel planes, with a constant flux on the upper boundary. Uniform initial distribution is considered. If diffusion-limited, the evolution of the electrical conductivity in response to a change in oxygen fugacity can be described by the following solution to the equation of one-dimensional diffusion:

$$\frac{\sigma(t) - \sigma_{initial}}{\sigma_{equilibrium} - \sigma_{initial}} = 1 - \sum_{n=0}^{\infty} \frac{8}{(2n+1)^2 \pi^2} \cdot \exp\left[\frac{-D(2n+1)^2 \pi^2 t}{4L^2}\right] \quad (7)$$

with $\sigma(t)$ the electrical conductivity ($ohm.m$)⁻¹ at time t (s), $\sigma_{initial}$ the electrical conductivity ($ohm.m$)⁻¹ at $t=0$, $\sigma_{equilibrium}$ the electrical conductivity ($ohm.m$)⁻¹ at $t=t_{eq}$, D the bulk diffusion coefficient (m^2/s), and L the length of the sample (m) (Crank, 1975, p.48). Eq.7 assumes a constant D as a function of time at a given temperature. The corresponding bulk redox front delimits the unreacted melt and is represented by ξ on Figure 6.

Experimental data on the changes of conductivity with time (Figures 5a; b) were fitted using Eq. 7 and bulk diffusivity values (D) were determined. This approach proved successful for the reduction experiments performed with CO-CO₂ and the oxidation experiments in air (Figure 5a; b), suggesting that both redox reactions are diffusion-limited processes. Calculated values of D are similar within uncertainties when determined at the same temperature, underlining that reduction and oxidation kinetics operate at the same rates (Figure 9a). In contrast, oxidation performed under CO₂ is not compatible with Eq.7 and, therefore, in this case the redox evolution is not rate-limited by diffusion (Figure 5c). In general, redox studies have been performed assuming that the processes studied are diffusion-limited. Our approach, consisting in following redox processes in real-time and with high accuracy, suggests that the nature of the gaseous oxygen carrier influences the redox kinetics and that, the redox processes under CO₂ are probably not diffusion-limited. A linear evolution of the electrical conductivity with time is clearly observed, independently of the gas flux. A few previous studies have reported non-diffusion-limited processes during redox experiments under pure CO₂ (Goldman, 1983; Goldman and Gupta, 1983; Schreiber et al., 1986; Roskosz et al., 2008). Most likely, the linear changes shown in Figure 5c reveal a specific rate-limiting process at the gas/melt interface (e.g. surface diffusion, chemical reaction).

The temperature dependence of the calculated D values follows an Arrhenian dependence (Figure 9a):

$$D = D_0 \cdot \exp\left[\frac{-E_{a_D}}{RT}\right] \quad (8)$$

with E_{a_D} the activation energy (kJ/mol) and D_0 the pre-exponential factor (m²/s). Our diffusivity values range from 10⁻⁹ to 10⁻⁸m²/s for the T range 1200-1400°C. These diffusion rates are comparable to typical alkali self-diffusion coefficients in basaltic melts from literature (Henderson, 1985; Chakraborty, 1995). Comparable diffusivity values are also calculated using the Nernst-Einstein equation (Eq. 5) and assuming that sodium is the unique charge carrier in the melt (i.e. $\sigma_{\text{equilibrium}} = \sigma_{\text{Na}^+}$). These two points underline the importance of the role of sodium in the investigated redox processes. However, the high values of activation energy ($E_{a_D} \geq 200$ kJ/mol, Figure 9a, b) calculated from Eq.8 are similar to activation energy for alkali-Earth elements (LaTourrette et al., 1996; Chakraborty, 1995) and oxygen self-diffusion (Leshner et al., 1996; Tinker et al., 2003) in silicate melts and is higher than the one expected for alkali self-diffusion (~100kJ/mol, Chakraborty, 1995) (see also Appendix 2).

Activation energy and pre-exponential term for redox kinetics in melts obtained in this study and previous ones (Lawless and Wedding, 1970; Sasabe and Goto, 1974; Doremus, 1960;

Dunn, 1983; Semkow and Haskin, 1985; Schreiber et al., 1986; Cook et al., 1990; Wendlandt, 1991; Cooper et al., 1996; Cook and Cooper, 2000; Everman and Cooper, 2003) are plotted in a compensation plot (Figure 9b). The compensation law for natural melts ($r^2 > 0.91$) is:

$$E_{aD} = 11.84 \cdot \ln D_0 + 293.5 \quad (9)$$

The single trend stresses that the kinetics of redox changes in our study is essentially similar to that found in other studies.

Figure 9c presents the calculated oxidation-reduction rates as a function of oxygen fugacity variations. Variations of fO_2 (initial fO_2 – final fO_2) are directly correlated to variations of the driving potential (or driving force, $\Delta\mu$) of the redox reaction occurring in the melt:

$$\Delta\mu = \Delta (R.T.\ln fO_2) \quad (10)$$

No clear evidence of such a dependence of D values is observed for our experiments, even for the experiments at 1300°C that involve the largest $|\Delta \log fO_2|$ (from 2 to 7). Figure 9c suggests that a possible dependence of D to variations of fO_2 is too weak to be discriminated and that the high D values calculated in our redox experiments can not be explained by variations of the driving potential.

5.3. Redox dynamics

Redox mechanisms are proposed on the basis of conductivity measurements, chemical titrations, mass balance calculations, EMPA profiles and previous redox studies. EMPA profiles (Figure 6) show complex pattern of chemical zonation, which are however difficult to interpret in terms of cation fluxes, since a change in cation content can be caused by the dilution effect of other mobile species. Microprobe traverses were nevertheless used to detect an internal reaction front, ξ' , whose location is presented in Figure 6. ξ' corresponds to an inflexion point in the chemical profiles.

ξ' is different from the bulk reaction front ξ'' provided by bulk diffusion coefficients (Eq.7). The identification of these two fronts stresses out two different steps of one reaction or two different reactions that are all part of the redox mechanisms. Position of ξ' at t corresponds to diffusivities in the melt of $\sim 10^{-11} \text{ m}^2/\text{s}$ for both reductions and oxidations, using the following equation:

$$D = L^2/t \quad (11)$$

D the diffusion coefficient (m^2/s), L defining the distance between ξ' and the gas/melt interface (m), t the time of quenching (s). These values are much lower than bulk diffusivities deduced

from conductivity measurements using Eq.7 (10^{-9} - 10^{-8} m²/s). The progression rate of ξ' compares well with self-diffusivities of O and Si in basaltic liquid (Canil and Muehlenbachs, 1990; Leshner et al., 1996) and with the rate laws derived by Cooper and coworkers using similar methodologies (identification of a migration front of cations). Another argument for O and Si mobility in the interface zone is that our E_{aD} values are comparable with E_a values from viscosity measurements (Giordano et al., 2008), which are based on the Si-O bonds (and oxygen mobility). The mobility of Si as Si-O has been previously suggested by Terai and Oishi, 1977. This suggests that Si-O mobility defines the progression of ξ' , which is not considered in the model of Cooper et al. (1996b). Si-O species are less mobile than sodium and they are not charged species. Thus, they do not directly influence the observed changes in conductivity. However, their migration could influence the charge carrier mobility. The effect of Si-O on σ would thus be indirect and part of the cations mobility can be interpreted as a consequence of Si-O migrations.

The progression rate of ξ' , graphically deduced from EMPA profiles, is slower than the progression rate of ξ'' , determined using electrical measurements and corresponding to the rate of the evolution of the redox ratio. This implies that apparent divalent cation migration and Fe^{2+}/Fe^{3+} changes are kinetically decoupled. This was not observed in previous studies that proposed redox mechanisms controlled by divalent cations mobility, since the time-evolution of the Fe^{2+}/Fe^{3+} ratio was not monitored in these studies (e.g., Cooper et al., 1996b). The rate laws of the evolution of ξ'' observed in our study are comparable to the kinetics of iron redox reactions in silicate melts (e.g. Magnien et al., 2008).

A schematic drawing of reduction and oxidation dynamics at the scale of the sample are proposed in Figure 10. The model considers the main fluxes of mobile species and, in particular, the rate-limiting ionic fluxes that probably hide other minor processes occurring at the same time. This implies that metastable structures that are probably formed during the initial stages of the redox reaction are not represented. We assume that the influence of these structures on the calculations of diffusion coefficients of mobile species during the redox reaction can be neglected. The model used to represent the evolution of a redox reaction is based on a Fickian formalism. This simple approach can be used as a first approximation which allows us to explain the D values in terms of major cation fluxes. The fluxes of cations (j_i) between the free surface (ξ_0) and the bulk reaction front ξ'' have been analyzed using the Fick-Einstein equation applied to ionic materials (Cooper et al., 1996a):

$$j_i = \frac{x_i \cdot D_i}{\lambda_i \cdot V_m \cdot \Delta \xi} \cdot \ln \left(\frac{f_{O_2}^{\xi=0}}{f_{O_2}^{\xi''}} \right) \quad (12)$$

with x_i the molar fraction of the cation i (Na^+ , K^+ , Ca^{2+} , Mg^{2+} , Fe^{2+}), D_i its diffusion coefficient (m^2/s), λ_i the stoichiometric coefficient, V_m the molar volume of the reduced or oxidized melt (m^3/mol), $\Delta \xi$ the distance between the free surface and the bulk reaction front (m), and f_{O_2} the oxygen fugacity (Pa) (with the superscript indicating location). The f_{O_2} ratio expresses the difference in oxygen chemical potential between reacted and unreacted melt (i.e. between ξ_0 and ξ''). D values for cations come from the literature (Henderson et al., 1985; Chakraborty, 1995; Lesher et al., 1996) and are assumed to be constant during the redox reaction. λ_i values correspond to the number of mol of cation in the oxidized form (molecular form) that is produced when one mole of O_2 reacts with cation i . Details on the calculations of λ_i are presented in Appendix 3. $\Delta \xi$ is calculated using Eq. 10 with $D=D_{\text{bulk}}$ (from Eq.7) and $t=t_{\text{quench}}$ (Table3).

In the case of redox mechanisms driven by a single kind of ionic species (e.g. divalents cations, Cooper et al., 1996), the motion of the redox front into the melt with time can be written as follows:

$$\frac{d\Delta \xi}{dt} = \lambda_{M^{2+}} \cdot j_{M^{2+}} \cdot V_m = \frac{x_{M^{2+}} \cdot D_{M^{2+}}}{\Delta \xi} \cdot \ln \left(\frac{f_{O_2}^{\xi_0}}{f_{O_2}^{\xi''}} \right) \quad (13)$$

M^{2+} being a divalent cation. These mechanisms were observed for experimental timescales of a few seconds or minutes (Cooper et al., 1996b; Everman and Cooper, 2003) or in the glass region (Cooper et al., 1996a; Cook and Cooper, 2000). As discussed before, at the timescale of our experiments (i.e. several hours), redox dynamics in the basaltic melts probably not come down to the only divalent cation fluxes. Our study suggests that oxygen, and alkalis also probably contribute significantly to the advancement of the bulk redox front ξ'' . The time-evolution of the redox front becomes:

$$\frac{d\Delta \xi}{dt} = \left(\sum_{M^{2+}} \lambda_{M^{2+}} \cdot j_{M^{2+}} + \sum_{A^+} \lambda_{A^+} \cdot j_{A^+} + \lambda_{O^{2-}} \cdot j_{O^{2-}} + \lambda_h \cdot j_h \right) \cdot V_m \quad (14)$$

with $M^{2+} = \text{Ca}^{2+}$, Mg^{2+} , Fe^{2+} , $A^+ = \text{Na}^+$, K^+ and h the electron holes. $\lambda_{M^{2+}} = \lambda_{A^+} = 2$, $\lambda_{O^{2-}} = 2$, $\lambda_h = 4$ (Appendix 3).

Si^{4+} and Al^{3+} ions are not considered in the present redox model. No evidence of free Si^{4+} ions has been found in previous studies (Bockris et al., 1952; Semkow and Haskin, 1985). The very high bond energy of Si-O ($\sim 373 \text{ kJ/mol}$, Bockris et al., 1952) strengthens the low probability for Si^{4+} ions to exist in a free state capable of migration within the melt. A significant role of aluminium in redox mechanisms has never been observed, to our knowledge.

The fluxes of considered cations are calculated using Eq.12 and the flux of oxygen can be expressed by:

$$j_{O^{2-}} = \frac{x_{O^{2-}} \cdot D_{O^{2-}}}{2 \cdot Vm \cdot \Delta \xi} \cdot \ln \left(\frac{f_{O_2}^{\xi=0}}{f_{O_2}^{\xi''}} \right) \quad (15)$$

where $x_{O^{2-}} = \frac{n_{oxygen}}{n_{total}}$. n_{oxygen} corresponds to the total oxygen content of the melt. n_{total} corresponds to the amount of oxygen and cations. Both n_{oxygen} and n_{total} are determined by mass balance calculations. As in Cooper et al. (1996a), the flux of electron holes (j_h) was calculated using the charge neutrality condition:

$$\sum_i z_i \cdot j_i = \left(\sum_{cations} z_{cations} \cdot j_{cations} \right) - 2j_{O^{2-}} + j_h = 0 \quad (16)$$

where $z_{cations}$ corresponds to the valence of the cations. Calculation of $d\xi/dt$ using Eq. 14 for the quenched experiments yields similar values for oxidation and reduction at the same temperature. For instance, $d\xi/dt = 2.2 \cdot 10^{-7} \text{ m/s}$ and $8 \cdot 10^{-8} \text{ m/s}$ for experiments #12-QO and #4-QR, respectively (Table 3).

As shown in Figure 10, the incorporation (oxidation) or release (reduction) of oxygen leads to competitive mechanisms between the different ionic species. At the internal front ξ' , variations of Na^+ mobility are related to the reduction or oxidation of ferric or ferrous iron, respectively. In oxidation and reduction experiments, the reacted melt (delimited by front ξ'') is characterized by opposite fluxes of oxygen and cations. The smaller amounts of network-modifier cations compared to oxygen anions imply electron holes to charge-balance O^{2-} fluxes.

According to Eq. 12 and 14, the evolution of the redox front as a function of time can be written as follows:

$$\Delta \xi \cdot d\Delta \xi = \sum_i A_i \cdot dt \quad \text{with} \quad A_i = x_i \cdot D_i \cdot \ln \left(\frac{f_{O_2}^{\xi_0}}{f_{O_2}^{\xi''}} \right) = \lambda_i \cdot j_i \cdot Vm \quad (17)$$

Integration of Eq. 17 leads to the following parabolic kinetic law:

$$\int_{\xi_0=0}^{\xi''} \Delta \xi . d\Delta \xi = \sum_i A_i . \int_{t_0=0}^t dt \Rightarrow \frac{\xi''^2}{t} = 2 . \sum_i A_i \quad (18)$$

The term $\frac{\xi''^2}{t}$ (in m²/s) corresponds to a bulk diffusion coefficient associated to the redox reaction and, thus, should be compared to the values of the redox front diffusion coefficient D_{bulk} calculated using Eq. 7. Numerical calculations yield values of $\frac{\xi''^2}{t}$ similar to the measured D_{bulk} (Eq.7 and Figure 9a): between $\sim 1.8 \cdot 10^{-9} \text{m}^2/\text{s}$ at 1200°C and $\sim 4.5 \cdot 10^{-9} \text{m}^2/\text{s}$ at 1300°C. This implies that the evolution of the redox front with time can be explained by a mechanism involving co-operative fluxes of cations, oxygen and electron holes. The contribution of cations and oxygen to the redox mechanisms are in agreement with the high activation energy values calculated using Eq.8 ($>200 \text{kJ/mol}$). The calculated fluxes of cation (Eq. 12) needed to match the global redox kinetics are however small (10^{-11} - $10^{-13} \text{mol.m}^{-2}.\text{s}^{-1}$). This is consistent with the absence of noticeable cations variations in the inner part of the quenched samples using EMPA profiles (distance $> \xi'$, see Figure 6). Highest values of fluxes correspond to oxygen and sodium ($\sim 10^{-11} \text{mol.m}^{-2}.\text{s}^{-1}$, whereas fluxes of potassium and divalent cations are $\sim 10^{-12}$ - $10^{-13} \text{mol.m}^{-2}.\text{s}^{-1}$), implying that these two species are the main contributors to the redox dynamics.

The mechanism that occurs to finally provide a uniform chemistry (e.g. from profile C to D in Figure 6) probably consists in a reequilibration of electrochemical potential. This reequilibration would correspond, in the case of our samples, to a coupled exchange of moving back alkali and divalent cations.

6. CONCLUSION AND REDOX EXCHANGES IN NATURE

Electrical measurements have been used to investigate in real-time redox kinetics in basaltic liquids after $f\text{O}_2$ -step changes. Data were recorded between 1200 and 1400°C, on the $f\text{O}_2$ range 10^{-8} -0.2 bars. Electrical conductivity was found to increase slightly with decreasing $f\text{O}_2$. A modified Arrhenius law expressing the dependence of the electrical conductivity to both $f\text{O}_2$ and T has been proposed. The evolution of electrical conductivity, based on sodium mobility, reproduces the evolution of the ferric/ferrous ratio of the melt. Reduction under CO-CO₂ and oxidation in air are diffusion-limited processes, whereas a gas-melt interface reaction probably rate-limit oxidation under pure CO₂. The high diffusion rates (10^{-9} - $10^{-8} \text{m}^2/\text{s}$) and activation

energies (>200 kJ/mol) calculated on the investigated T range in basaltic melts can be explained by redox mechanisms involving co-operative alkali, divalent cations and oxygen fluxes.

According to Gaillard et al. (2003a), attainment of redox equilibrium in hydrogen-bearing melts was found to be rate-controlled by H₂ fluxes in the melt at a reaction front corresponding to:



This statement was particularly supported by the fact that H₂ migration in the melt is much faster than divalent cations migration calculated after Cooper and coworkers. For example, at 1300°C, at f_{H2}=1 and 100bar, Gaillard et al. (2003a) calculated reaction rates of iron redox changes in hydrous magmas of ~2.5.10⁻¹² and 10⁻⁹ m²/s, respectively, while extrapolation of D values of Cooper et al. (1996a) at the same T in basaltic melts provides a reaction rate of ~4.10⁻¹³ m²/s. Our results, however, indicate reaction rates of 10⁻⁹-10⁻⁸m²/s at 1300°C, which exceed well the rates extrapolated from Cooper et al (1996a). The hydrogen-dominated mechanisms exposed in Gaillard et al. (2003a) will therefore not necessarily operate in basaltic systems because cooperative motions of oxygen and cations revealed in our study can be faster than exchanges rate-limited by H₂ fluxes. Only for fH₂ values exceeding 50 bars, reaction rates are nearly equivalent, implying that the mechanisms of Gaillard et al. might affect basalts under specific conditions such as in moderately oxidized mantle wedge (water-rich at NNO). However, in most conditions experienced by basaltic liquids (i.e. moderately hydrated), the mechanism we revealed in our study should dominate the kinetics of redox potential re-equilibration.

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Appendix 1: On the difference between oxygen self-diffusion (D^*) and chemical diffusion (D) coefficients

As underlined by Cooper et al. (1996a), two kinds of experiments are commonly used to study diffusion-limited oxidation/reduction kinetics: oxygen self-diffusion and chemical diffusion (redox) experiments. By “chemical diffusion experiments”, we consider experiments that let the sample equilibrate with a change in the gaseous atmosphere. The diffusing species, depending on the authors, are oxygen or cations or both (this study). By “oxygen self-diffusion experiments”, we consider experiments (mainly isotopic) that study the tracer (or network) diffusion of oxygen. As shown in the following Figure A, several orders of magnitude separate values of chemical diffusion coefficients and oxygen self-diffusion coefficients for similar silicate melts compositions ($D > D^*$). For example, in a basaltic melt at 1300°C, in air, the self-diffusion coefficient of oxygen is estimated at $\sim 6.5 \cdot 10^{-12} \text{ m}^2/\text{s}$ (Canil and Muehlenbachs, 1990) while we calculated from our study a bulk chemical diffusion coefficient of $\sim 3.5 \cdot 10^{-9} \text{ m}^2/\text{s}$.

Differences have been interpreted in terms of diffusion mechanisms, chemical diffusion involving the diffusion of molecular oxygen, vacancies or cations and tracer diffusion involving the migration of ionic species (Schreiber et al., 1986; Wendlandt, 1991; Cooper et al., 1996a).

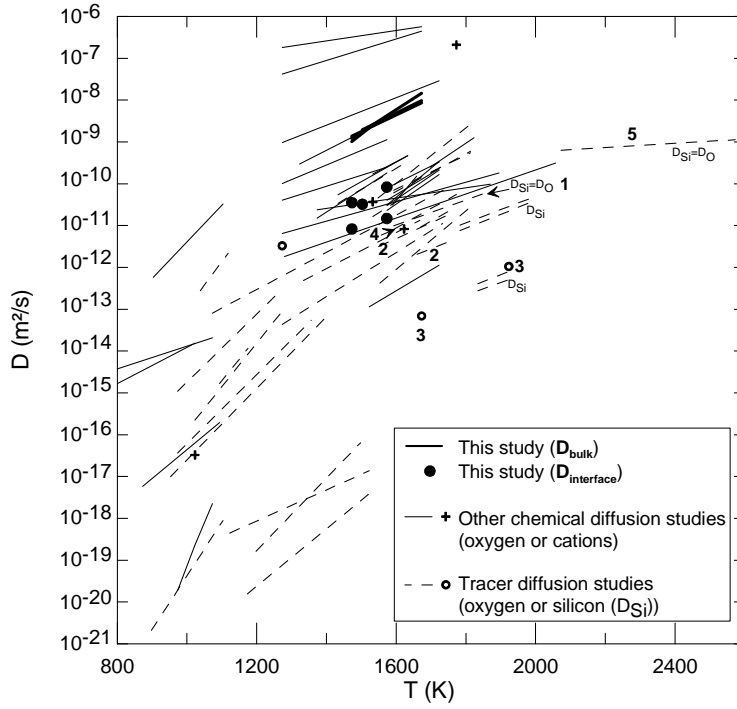


Figure A: Comparison between chemical diffusion experiments and oxygen self-diffusion experiments. Diffusion coefficients as a function of temperature. Data from this study (bold full lines and filled circles) and other chemical diffusion studies (full lines and crosses) and tracer diffusion studies (dashed lines and empty circles). Data are taken from this study and from May *et al.* (1974) and references therein; Schreiber *et al.* (1986) and references therein; Canil and Muehlenbachs (1990); Cook *et al.* (1990); Wendlandt (1991); Cooper *et al.* (1996); Cook and Cooper (2000); Smith and Cooper (2000); Reid *et al.* (2001); Everman and Cooper (2003); Magnien *et al.* (2008). 1: Tinker *et al.* (2003) and Lesher *et al.* (1996); 2: Dunn (1982); 3: Shimizu and Kushiro (1984); 4: Canil and Muehlenbachs (1990); 5: Reid *et al.* (2001).

Appendix 2: Estimation of a normalized driving force

Another way to interpret the temperature-dependence of diffusivity values is to consider a normalized driving force $\Delta G/RT$. Over the investigated T range, this normalized driving force ranges from 21 at 1473K to 16 at 1673K (223/10.6 and 223/13.9, respectively). Using the following equation (Schmalzried, 1984),

$$k' = \lambda \cdot D' \cdot (\Delta G/RT) \quad (A0)$$

an average diffusion coefficient D' can be deduced; k' is the reaction-rate constant (i.e. the one resulting from our electrical measurements) and λ is a stoichiometric factor. In Evermann and Cooper, 2003, λ is taken as 5. If we consider that λ is related to the motion of oxygen, $\lambda = 2$ (cf Appendix 3).

For instance, at 1473K, $k' \sim 10^{-9} \text{ m}^2/\text{s}$. Depending on the value of λ , $D' = 2.3 \cdot 10^{-11}$ or $1 \cdot 10^{-11} \text{ m}^2/\text{s}$. These D' values are consistent with self-diffusivity values for divalent cations but also for oxygen in basaltic melts (cf Fig. 10.18 in Mysen and Richet, 2005). These calculations underline that fluxes of divalent cations and oxygen probably also contribute to the redox dynamics, cooperating with alkali fluxes.

Appendix 3: Relation of the mobile species fluxes to the evolution of the inner redox front

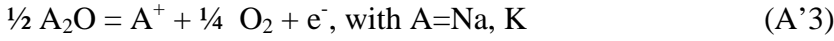
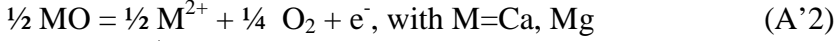
Redox processes in magmas can be expressed by changes of the ferric/ferrous ratio (Kress and Carmichael, 1988; Dunn and Scarfe, 1986). The corresponding equilibrium can be written as follows:



The quantity of oxygen consumed or produced in (A1) has direct implications on the structure of the melt and other cations configuration. These cations are considered to be present in the melt under molecular and ionic forms, what can be written by the following equilibria:



Or, rescaling to the stoichiometric coefficient of oxygen in (A1):



We can define the amount of cation in the oxidized form (molecular form) that is produced when one mole of O_2 reacts with cation i (ionic form) by the following stoichiometric coefficients λ :

$$\lambda_{\text{M}^{2+}} = \lambda_{\text{A}^+} = 2$$

Regarding oxygen anion, the reaction to consider is:



what leads to $\lambda_{\text{O}^{2-}} = 2$.

Finally, the stoichiometric coefficient corresponding to the electron holes contribution in the redox process can be evaluated using the following equilibria:



(A5) implies $\lambda_{\text{h}^+} = 4$.

The evolution of the inner redox front with time can thus be written as:

$$\begin{aligned} \frac{d\xi}{dt} &= \left(\sum_{\text{M}^{2+}} \lambda_{\text{M}^{2+}} \cdot j_{\text{M}^{2+}} + \sum_{\text{A}^+} \lambda_{\text{A}^+} \cdot j_{\text{A}^+} - j_{\text{O}^{2-}} + j_{\text{h}^+} \right) \cdot Vm \\ &= \left(\sum_{\text{M}^{2+}} 2 \cdot j_{\text{M}^{2+}} + \sum_{\text{A}^+} 2 \cdot j_{\text{A}^+} + 2 j_{\text{O}^{2-}} + 4 j_{\text{h}^+} \right) \cdot Vm \end{aligned}$$

Table 1: Composition of the starting glasses (in wt %). Figures into brackets correspond to the concentrations of major oxides in mol %.

Sample	VES9		Kilauea	
SiO ₂	49.2	(54.6)	50.0	(55.2)
TiO ₂	0.96	(0.80)	2.41	(2.00)
Al ₂ O ₃	15.1	(9.90)	13.2	(8.62)
FeO	1.73	(1.61)	3.16	(2.92)
Fe ₂ O ₃	6.08	(2.54)	8.58	(3.57)
MnO	0.20	(0.19)	0.13	(0.12)
MgO	6.26	(10.3)	7.50	(12.3)
CaO	11.5	(13.6)	10.6	(12.5)
Na ₂ O	1.97	(2.12)	2.29	(2.45)
K ₂ O	5.98	(4.23)	0.38	(0.27)
F	0.14		-	
Cl	0.12		-	
S	0.05		-	
Total	99.7	(100)	97.89	(100)
NBO/T	0.73		0.80	

Table 2: Conditions and results of the conductivity experiments.

Run	Sample	Initial conditions (Step 1)					Final conditions (Step 2)								
		T(°C)	Gas	log fO ₂ [◇]	ΔNNO	Duration (min)	T(°C)	Gas	log fO ₂ [◇]	ΔNNO	Duration (min)	σ eq (ohm.m) ⁻¹	t eq (min) ^a	at. Fe ²⁺ /Fe ³⁺	
Reduction															
#1	Ves	1200	CO ₂	-3.74	4.00	1050	1200	CO-CO ₂	-6.30	1.40	1650	0.63	1042	1.24	
#2	Ves	1250	CO ₂	-3.50	3.70	1320	1250	CO-CO ₂	-5.80	1.40	630	0.82	491	2.00	
#4	Kil	1200	CO ₂	-3.74	4.00	1370	1200	CO-CO ₂	-6.30	1.40	1410	1.00	778	2.24	
#5	Kil	1200	CO ₂	-3.74	4.00	1290	1200	CO-CO ₂	-7.25	0.45	1860	1.04	874	-	
#6	Kil	1300	CO ₂	-3.24	3.45	280	1300	CO-CO ₂	-5.31	1.35	430	1.50	203	-	
#7	Kil	1300	CO ₂	-3.24	3.45	1010	1300	CO-CO ₂	-6.70	0.00	290	1.65	124	2.55	
#8	Kil	1300	Air	-0.69	6.00	200	1300	CO-CO ₂	-7.67	-1.00	230	1.83	118	2.41	
#9	Kil	1400	Air	-0.69	5.10	200	1400	CO-CO ₂	-4.98	0.75	180	2.99	86.5	1.64	
#10	Kil	1400	Air	-0.69	5.10	190	1400	CO-CO ₂	-6.12	-0.35	80	3.10	72.5	-	
Oxidation															
#1rev	Ves ¹	1200	CO-CO ₂	-6.30	1.40	1650	1200	CO ₂	-3.74	4.00	2500	0.60	2500	1.00	
#5rev	Kil ²	1200	CO-CO ₂	-7.25	0.45	1860	1200	CO ₂	-3.74	4.00	1030	0.81	1000	1.58	
#6rev	Kil ³	1300	CO-CO ₂	-5.31	1.40	430	1300	CO ₂	-3.24	3.45	1530	1.27	1200	1.46	
#7rev	Kil ⁴	1300	CO-CO ₂	-6.70	0.00	290	1300	CO ₂	-3.24	3.45	910	1.42	720	1.47	
#12	Kil*	1400	CO-CO ₂	-4.98	0.75	100	1230	Air	-0.69	6.73	1380	0.98	560	0.37	
#13	Kil*	1400	CO-CO ₂	-6.12	-0.35	100	1230	Air	-0.69	6.84	1350	0.95	735	0.32	
#14	Kil*	1400	CO-CO ₂	-4.98	0.75	100	1300	Air	-0.69	6.00	1300	1.26	472	0.52	
#15	Kil	1300	CO-CO ₂	-6.70	0.00	260	1300	Air	-0.69	6.00	380	1.11	250	-	
#10rev	Kil ⁵	1400	CO-CO ₂	-6.12	-0.35	80	1400	Air	-0.69	5.10	200	2.18	111	0.69	

¹⁻⁵ Reduction reverse (Starting glass is final glass from a reduction experiment; Both have the same run number).

* Initial fO₂ step performed at T=1400°C>T of conductivity experiment (Final conditions) in order to increase the kinetics of the reduction phase.

◇ fO₂ in bar.

^a Time necessary for σ(t)=σ eq (plateau value), calculated as t=L²/D, with L=length of the glass sample.

Table 3: Conditions and results of the analytical experiments.

Run	Sample	Initial conditions (Step 1)					Final conditions (Step 2)						
		T(°C)	Gas	log fO ₂ [◇]	ΔNNO	Duration (min)	at. Fe ²⁺ /Fe ³⁺	T(°C)	Gas	log fO ₂ [◇]	ΔNNO	Duration (min)	
<i>Reduction</i>													
#4-QR	Kil	1200	CO ₂	-3.74	4.00	1000	0.95	1200	CO-CO ₂	-6.30	1.40	300	
#5-QR	Kil	1200	CO ₂	-3.74	4.00	1000	0.95	1200	CO-CO ₂	-7.25	0.45	45	
#6-QR	Kil	1300	CO ₂	-3.74	4.00	1000	0.80	1300	CO-CO ₂	-5.31	1.35	45	
<i>Oxidation</i>													
#12-QO	Kil	1230	CO-CO ₂	-6.30	1.40	900	-	1220	Air	-0.69	6.00	330	
#14-QO	Kil ¹	1400	CO-CO ₂	-4.98	0.75	100	-	1300	Air	-0.69	6.00	200	

* Duration of Step 2 corresponds to t_{quench}.

¹ This experiment is to be compared with experiment #14 in Table 2, although the difference in T regarding the initial conditions.
◇ fO₂ in bar.

Table 4: Arrhenius parameters for the investigated samples.

Gas (kJ/mol)	Log fO ₂ [◇]	ΔNNO	Fe ²⁺ /Fe ³⁺ (%at)	Lnσ ₀ (ohm.m) ⁻¹	Ea _σ
<i>Mt. Vesuvius sample (T range [1200-1250°C])</i>					
CO-CO ₂ mixture 1	[-6.30; -5.80]	~1.40	[1.24;2.00]	7.57	98
<i>Kilauea sample (T range [1200-1400°C])</i>					
Air	0.68	~7	[0.32;0.92]	7.21	90
CO ₂	[-3.74; -3.24]	[3.45; 4.00]	[1.22;1.58]	9.16	114
CO-CO ₂ mixture 1	[-6.30; -4.98]	[0.75; 1.40]	[1.64;2.24]	9.20	113
CO-CO ₂ mixture 2	[-7.25; -6.12]	[-0.35; 0.45]	2.55*	9.16	112

[◇] fO₂ in bar.

*one wet chemical analysis (run #7 in Table 2).

Figure captions

Figure 1: Description of (A) the conductivity cell and (B) the sample configuration for analytical experiments. The arrows represent the exchange with the gaseous atmosphere at the unique interface sample/gas. The straight lines represent the three types of microprobe traverses performed after the redox experiments (see text).

Figure 2: Electrical response observed in the Nyquist plan (Z' , Z'') for the Kilauea basalt at 1300°C, during oxidation in air. The first part of the response ($Z' < R$) represents the electrical response of the sample while the second part ($Z' > R$), represents the effect of the interface between the sample and the electrode. R (resistance of the sample (ohm)) is obtained for $Z'' = 0$ and represents the real part of the complex impedance (here, $R \sim 18.5 \text{ ohm}$).

Figure 3: Iron losses, example of the redox experiment at 1200°C (run #5). A: Molar fraction of metallic iron in the Pt electrode after. The EMPA profile shows that iron contamination affects the electrode on a distance $< 100 \mu\text{m}$. B: Concentration of total iron in mol of oxide normalized to 100. No noticeable iron depletion is detected in the sample, even at the interface glass/Pt electrode. Error estimation is presented in the box.

Figure 4: Electrical conductivity at the chemical equilibrium of the Kilauea sample as a function of oxygen fugacity, for T ranging from 1200°C to 1400°C. The conductivity slightly increases with decreasing the $f\text{O}_2$. The electrical conductivity is more strongly dependent on T than $f\text{O}_2$. Experimental conditions are indicated in Table 2. Dashed lines correspond to Eq.4. The electrical conductivity of the PG-16 basaltic melt at 1400°C from Waff and Weill (1975) (WW75) is shown for comparison.

Figure 5: Conductivity transients in oxidation and reduction reactions. A: Reduction example (run #6); B: Oxidation example (run #15). The solid lines correspond to the calculated conductivity with the diffusion equation of Crank (see text). C: Advancement of oxidation reaction in air and CO_2 as a function of time. The diffusion profile obtained in air contrasts with the more linear trend obtained under CO_2 . Triangles and diamonds underline that the non diffusion kinetics under CO_2 is not function of the gas flow in the furnace. Straight line is just a guide for the eyes.

Figure 6: Microprobe traverses from the gas/sample interface in Kilauea samples quenched during redox experiments and after conductivity experiment. A) 1300°C, $\log f\text{O}_2 = -5.31$, $t_{\text{quench}} = 45 \text{ min}$ (run #6-QR); B) 1200°C, $\log f\text{O}_2 = -6.30$, $t_{\text{quench}} = 300 \text{ min}$ (run #4-QR); C) 1300°C, $\log f\text{O}_2 = -0.68$, $t_{\text{quench}} = 300 \text{ min}$ (run #14-QO); D) 1230°C, $\log f\text{O}_2 = -0.69$ (run #12). Traverse D stresses that chemical compositions of starting glass and glass after the conductivity experiment are similar. Oxides concentrations are given in mol %. Variations in oxides concentrations allow to distinguish an interface zone, from the interface with gas to ξ' (dashed line, approximate localisation). The second internal front, ξ'' , delimiting the unreacted melt, is calculated using D values from Eq.7 (see text for details).

Figure 7: A) Ferrous-ferric ratio with ΔNNO for conductivity and analytical experiments performed on the Kilauea sample. See Tables 2 and 3 for experimental conditions. B) Equilibration time as a function of the ferrous-ferric ratio for the Kilauea sample. Examples of a reduction at 1200°C, $\log f\text{O}_2 = -6.30$ and of an oxidation at 1300°C, in air. The small error bars underline the high reproducibility of the wet chemical analyses. Crosses represent the

attainment of chemical equilibrium (plateau value), determined using electrical measurements (see text for details). The curves are just a guide for the eye.

Figure 8: Comparison between the evolution of the electrical response of the sample and the evolution of the ferrous-ferric ratio (in %). Data points fall on the straight line 1:1, indicating similar kinetics of the evolution of the conductivity and of the redox ratio in the melt.

Figure 9: Calculated bulk diffusivity values. A) Diffusion coefficients calculated using the equation of diffusion (Eq. 7, cf Crank, 1975, p.48) vs temperature. Data are presented for both reduction (open diamonds: VES sample; filled diamonds: Kil sample) and oxidation (stars, Kil sample). Experimental conditions are detailed in Table 2. The general regression (straight line) yields a correlation factor of 0.81, underlining similar kinetics for both reduction and oxidation. The similar D values for the two basaltic samples can be explained by the small differences in the chemical compositions (Table 1). B) Compensation plot for the diffusion coefficients from this study (triangles, calculated using Eq. 7) and from other studies, attributed to either the diffusion of oxygen or of divalent cations (D: Dunn, 1983; W: Wendlandt, 1991; C et al. 96: Cooper et al., 1996; EC: Everman and Cooper, 2003; Do: Doremus, 1960; LW: Lawless and Wedding, 1970; SG: Sasabe and Goto, 1974; SH: Semkow and Haskin, 1985; S et al.: Schreiber et al., 1986; CC: Cook and Cooper, 2000; C et al. 90: Cook et al., 1990). Data for natural and synthetic silicate melts. The dashed line represents the compensation law for natural melts (Eq.9). C) Calculated diffusing rates as a function of oxygen fugacity variations (proportional to the driving potential). Data at 1200°C (Kilauea and Mt Vesuvius samples), 1300°C and 1400°C (Kilauea sample).

Figure 10: Redox dynamics in the Kilauea basalt in the T range 1200-1400°C. Both reduction and oxidation involve chemical reactions at the free surface of the sample (ξ_0) and at two internal fronts (ξ' and ξ''). At ξ_0 , oxygen is released or incorporated in the melt, with h^\cdot being consumed or absorbed, respectively. At the internal front (ξ'), Fe^{3+} is reduced to Fe^{2+} (reduction) or Fe^{2+} is oxidized to Fe^{3+} (oxidation), implying variations on Na^+ mobility, and thus on the electrical response of the melt (see text for details). The measured bulk diffusion coefficient corresponds to the second internal front (ξ''). Competitive mechanisms occur between oxygen and cations diffusion. The smaller amounts of network-modifier cations compared to oxygen anions imply electron holes to charge-balance O^{2-} fluxes. The high diffusivities of h^\cdot probably enhance oxygen and cations diffusion, since the D values are deduced from electrical measurements and are thus related to charged mobile species. Oxygen probably moves in the melt as both ionic (O^{2-}) species, as underlined by several studies (e.g. Goldman and Gupta, 1983; Dunn, 1983; Schreiber et al., 1986; Wendlandt, 1991) and as oxide species, since spectroscopic studies showed that most bridging oxygens have cations in their first coordination shell, forming Q species (e.g. Stebbins, 1995).

Figure 1

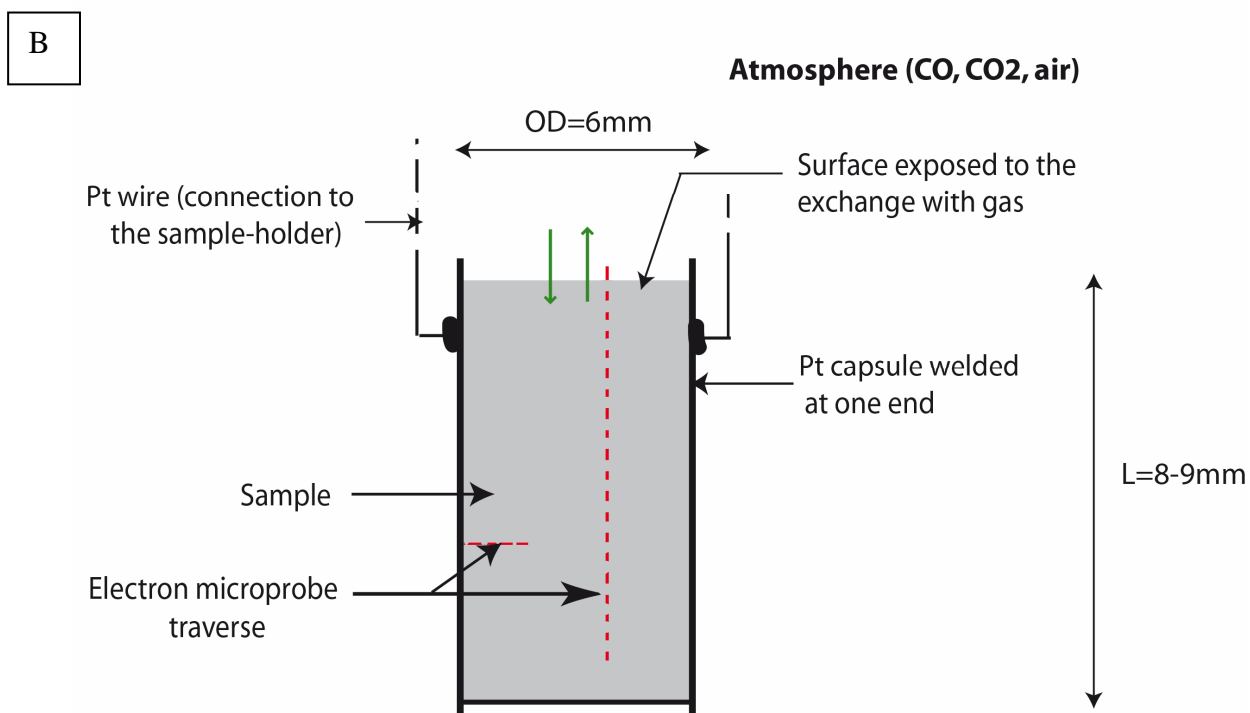
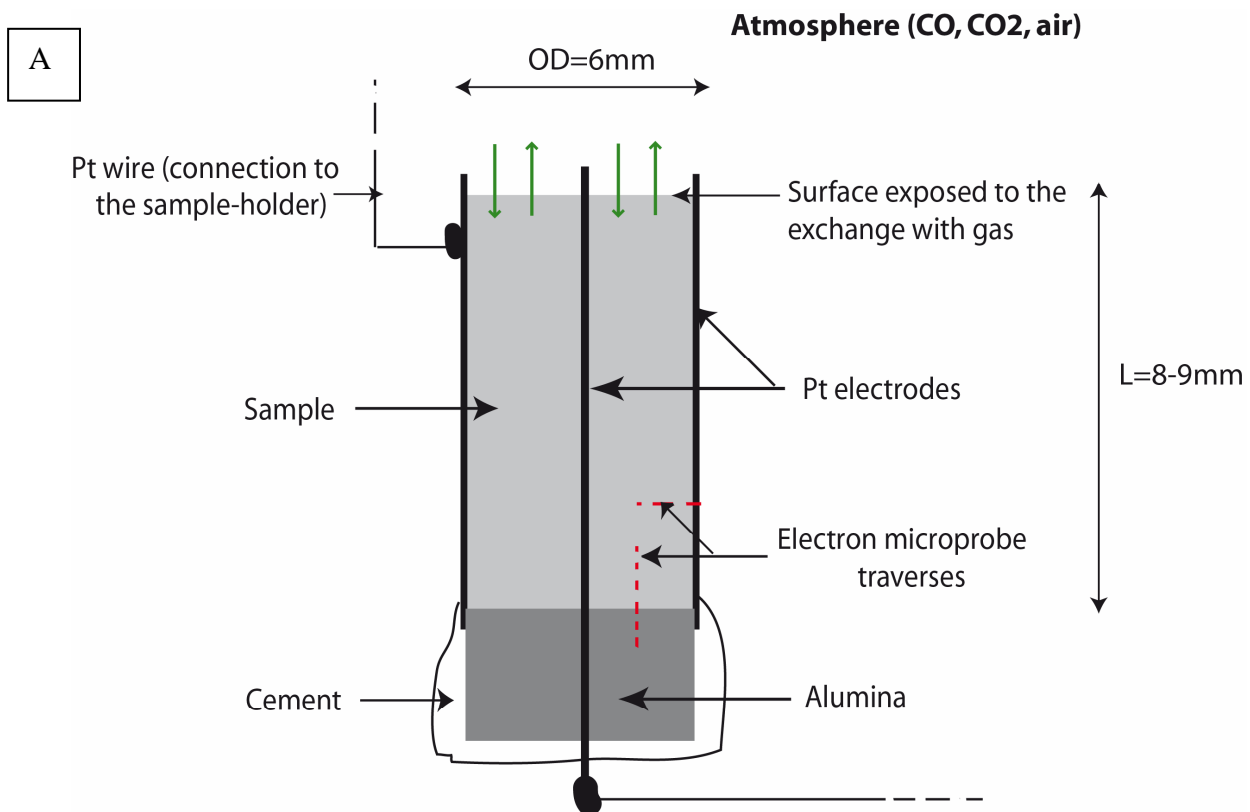


Figure 2

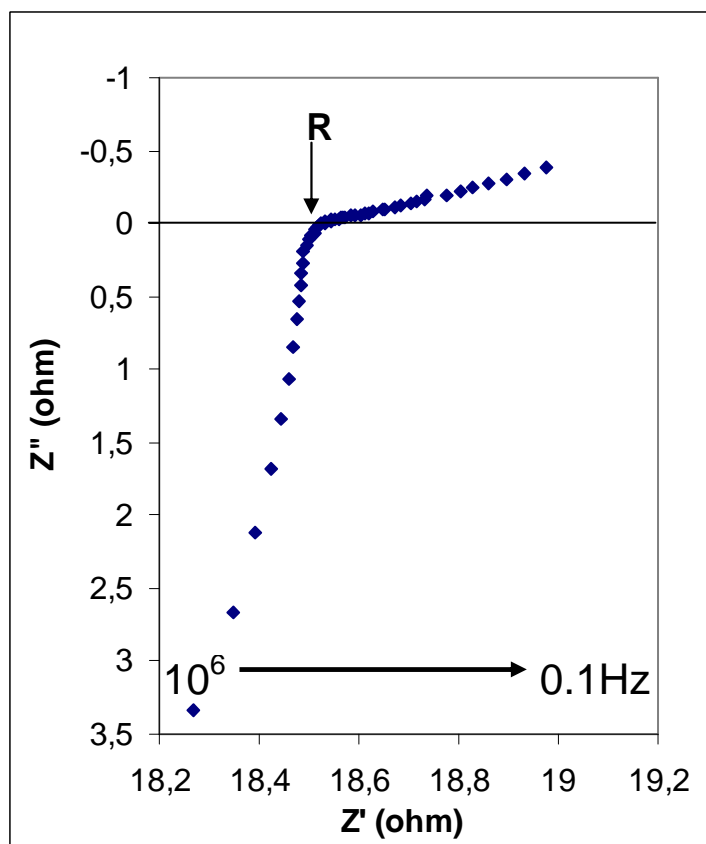
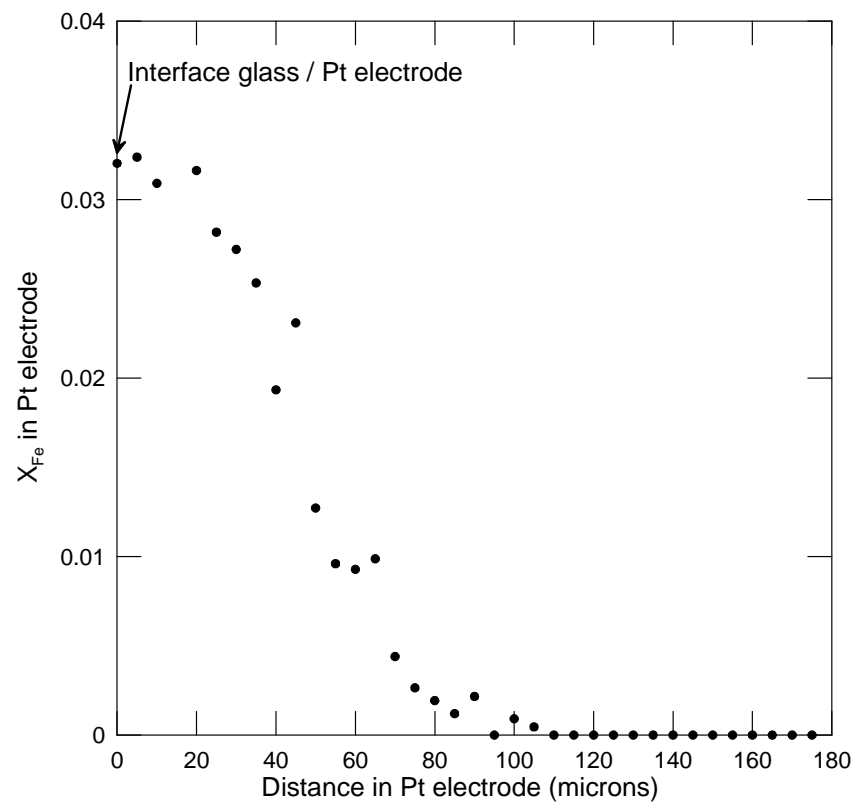


Figure 3

A)



B)

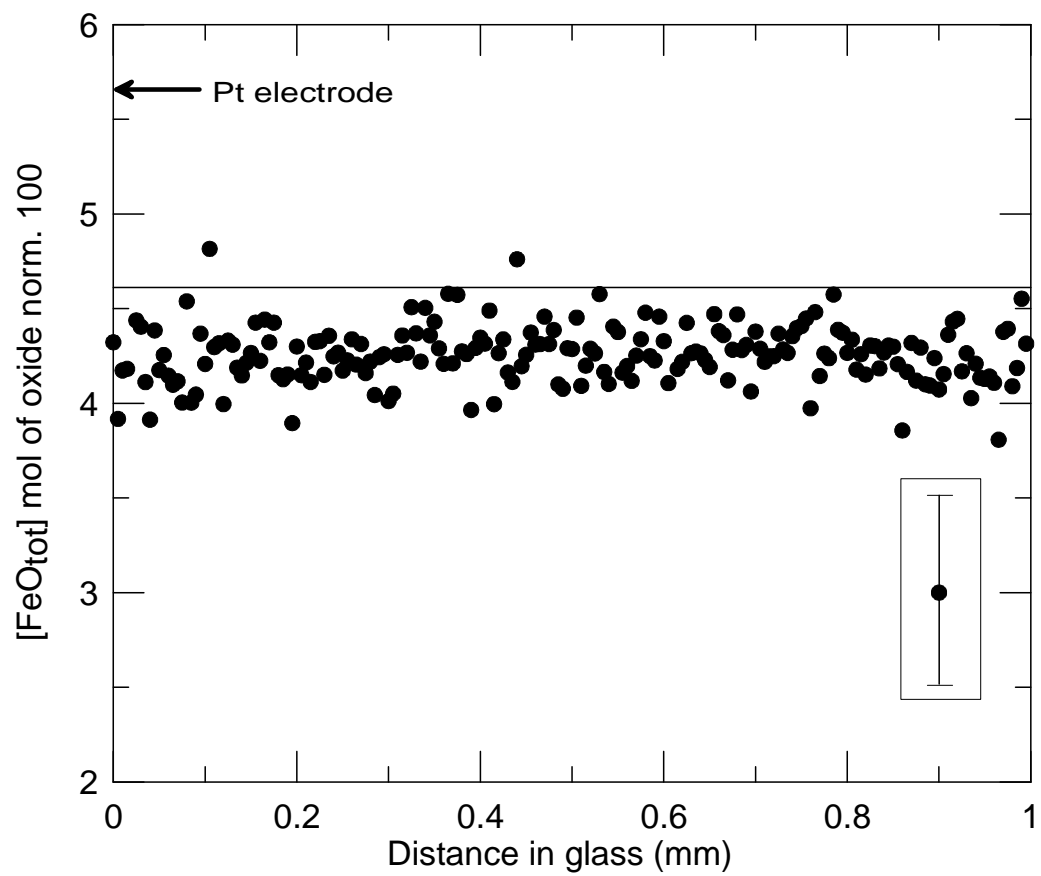
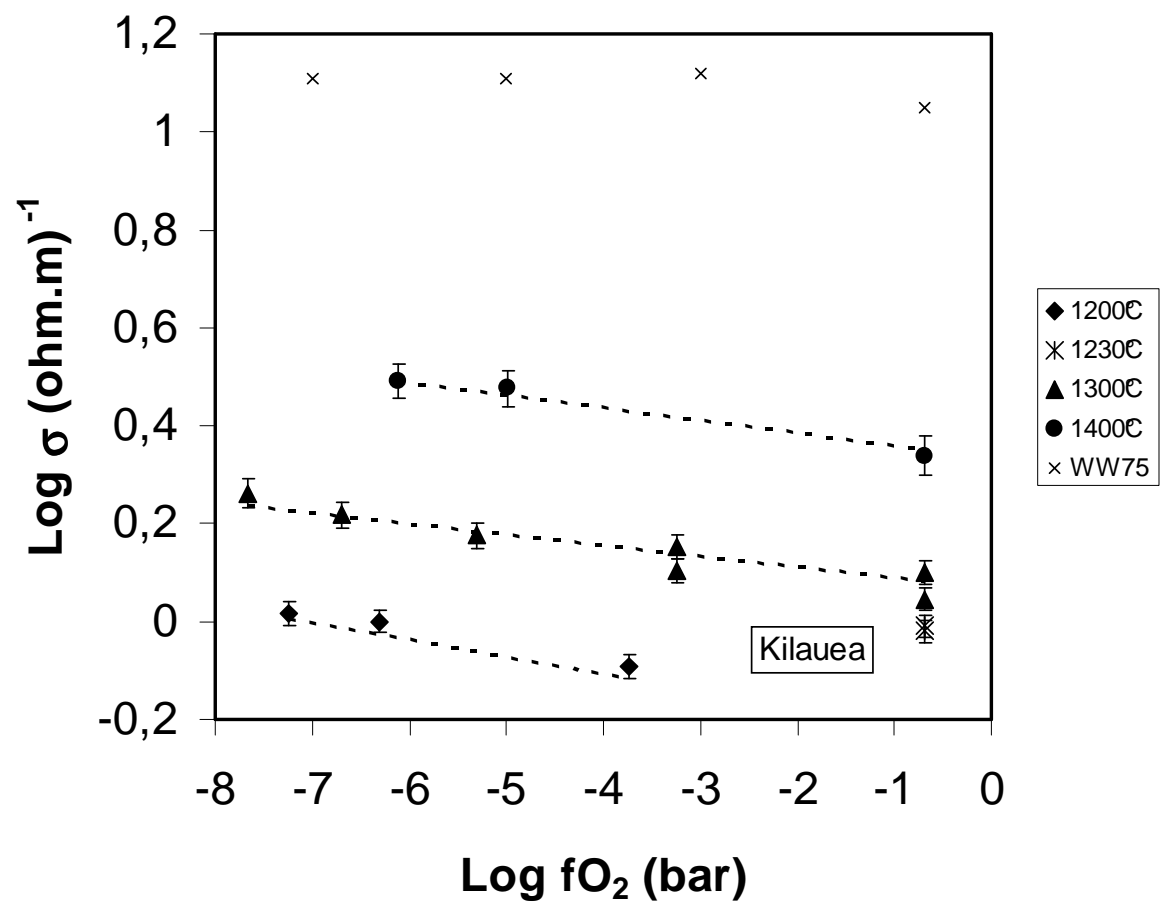


Figure 4



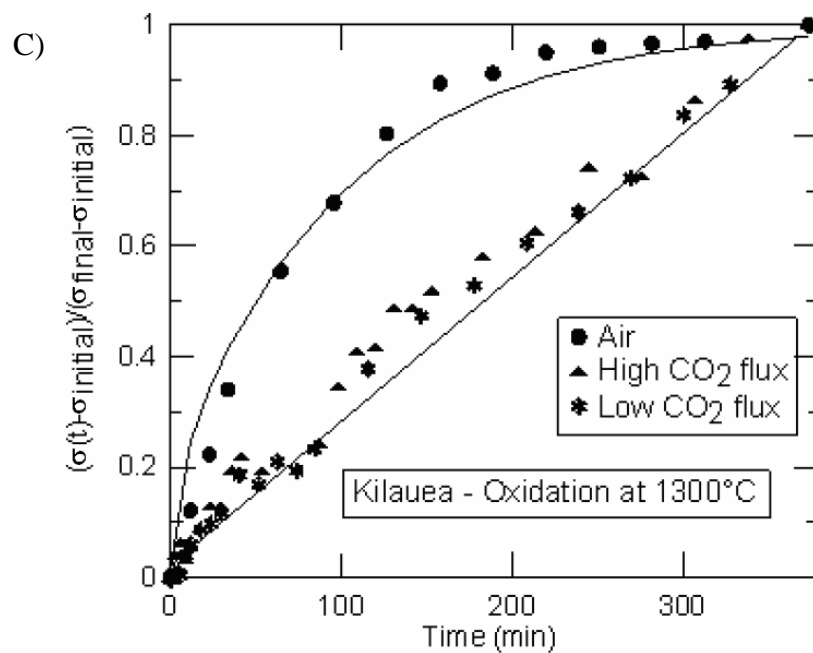
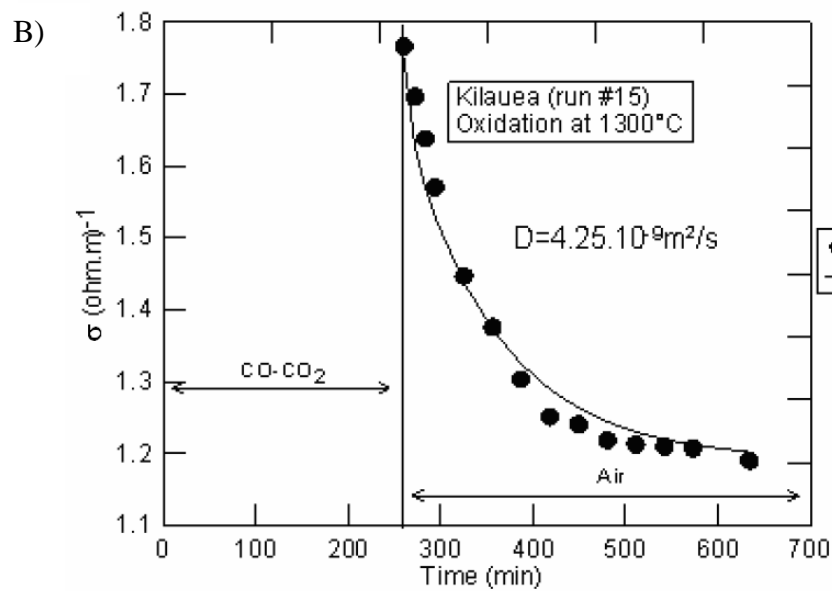
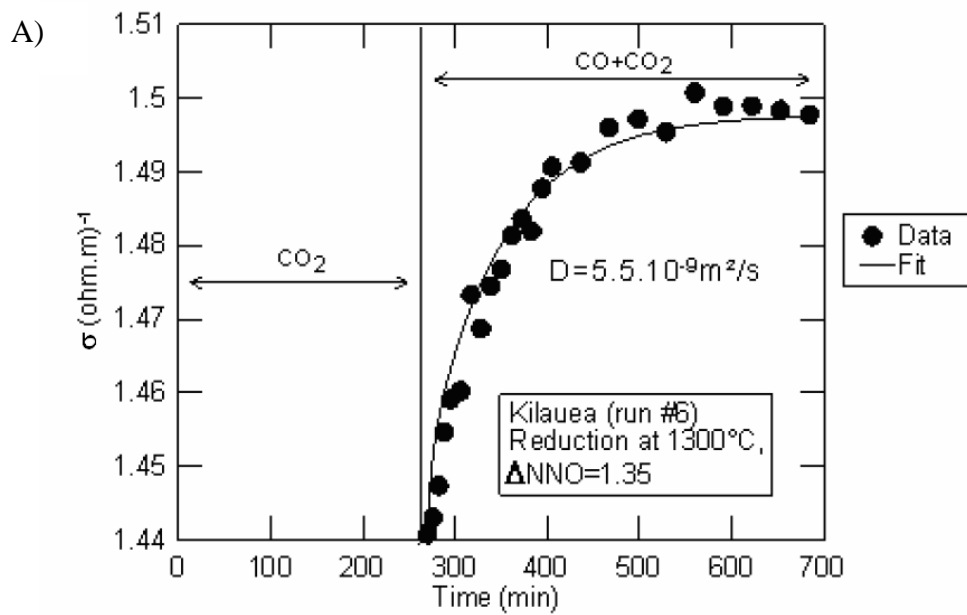


Figure 6

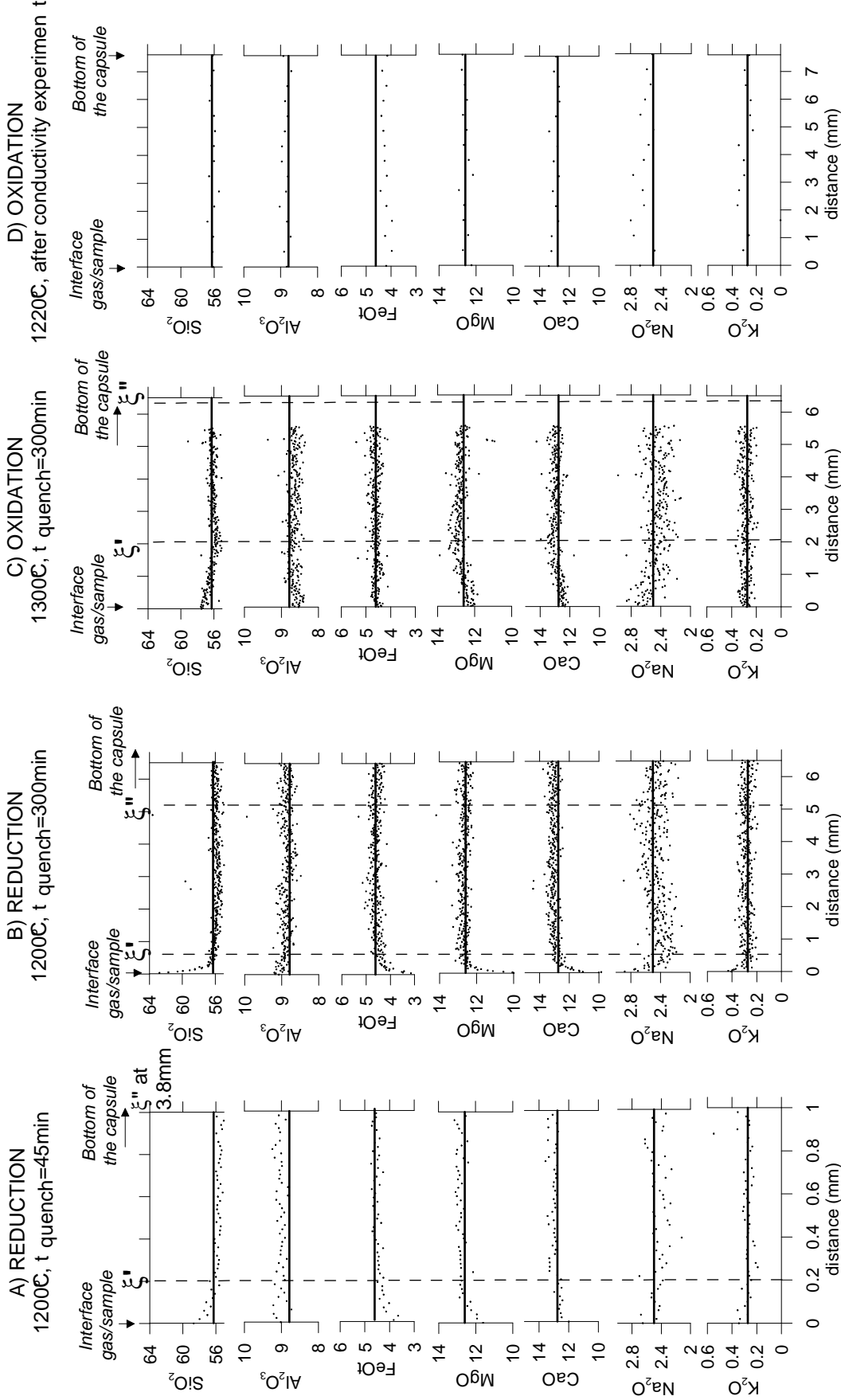
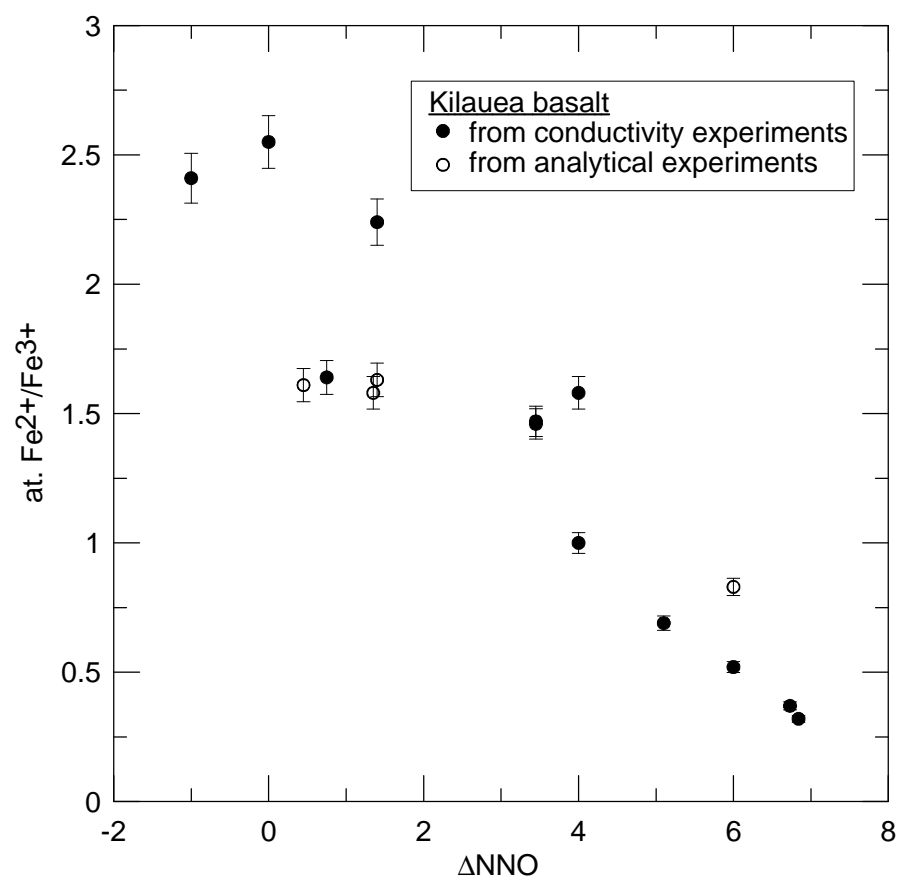


Figure 7

A)



B)

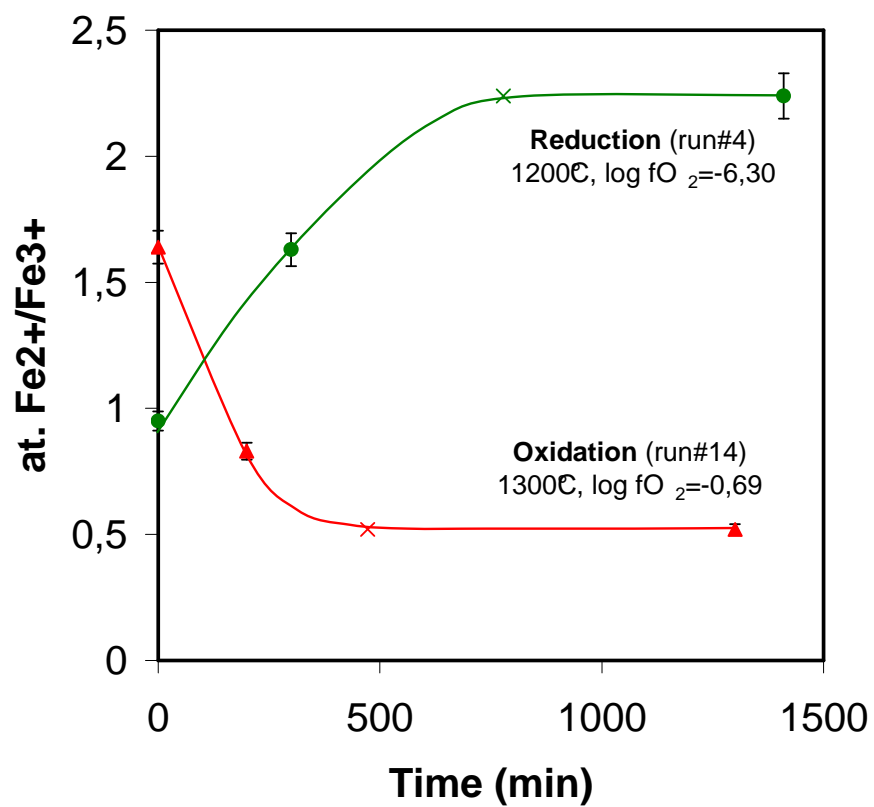


Figure 8

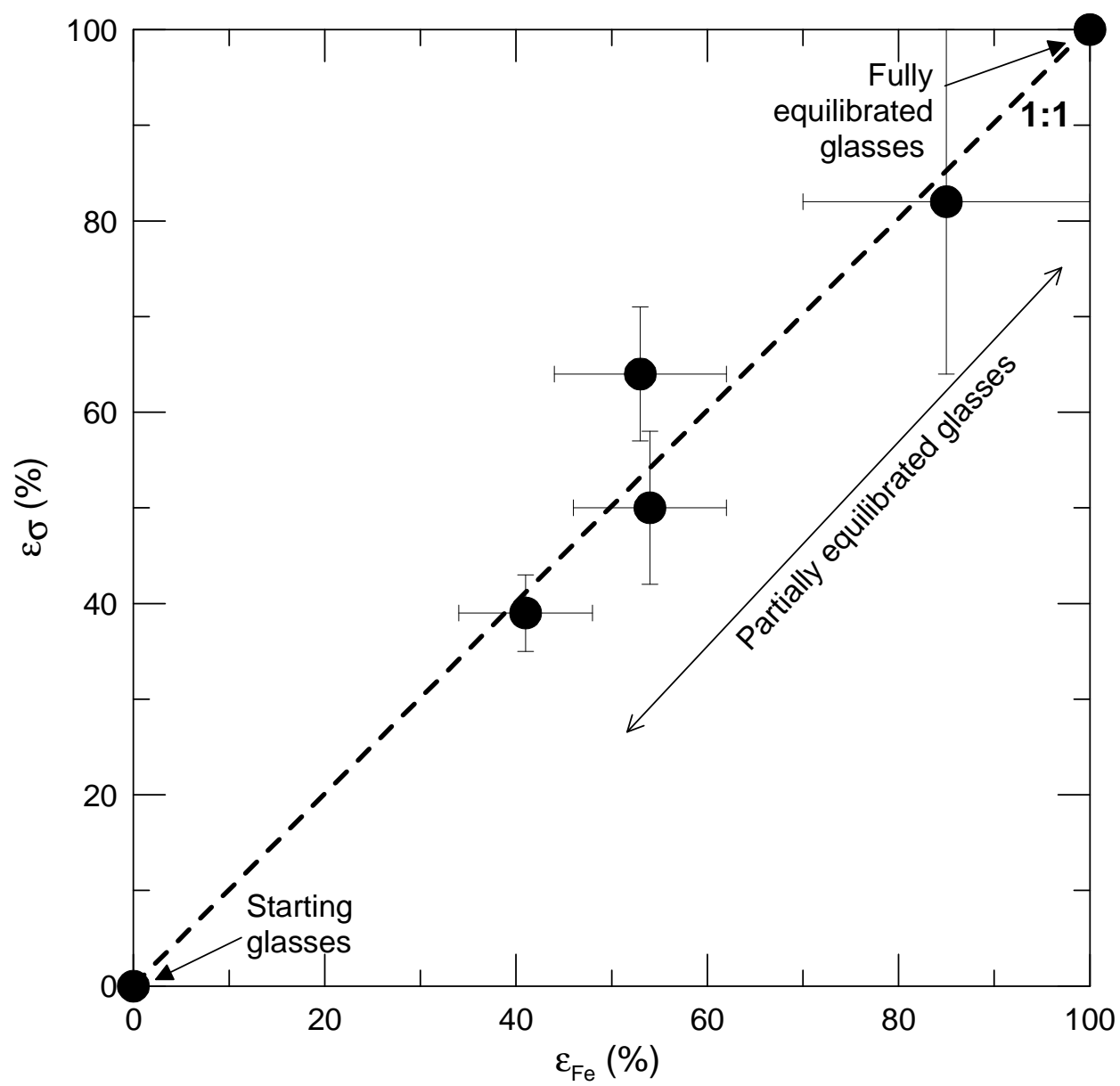
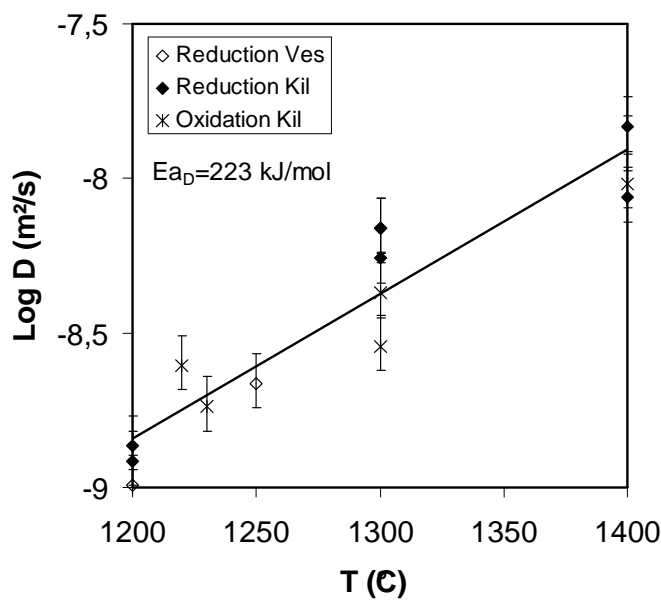
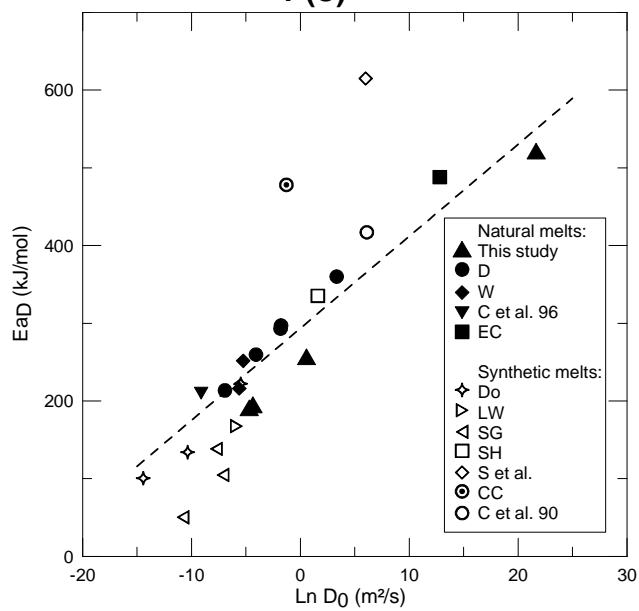


Figure 9

A



B



C

